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**IGCC**

**- 가 -**

2001. 12. 13.

Plant Engineering

**IGCC**

(311 )

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**IAE**

# 가

## □ 가

- SOx, NOx , H2S, NH3
- 
- 
- Dioxin
- 가

## □ Ash

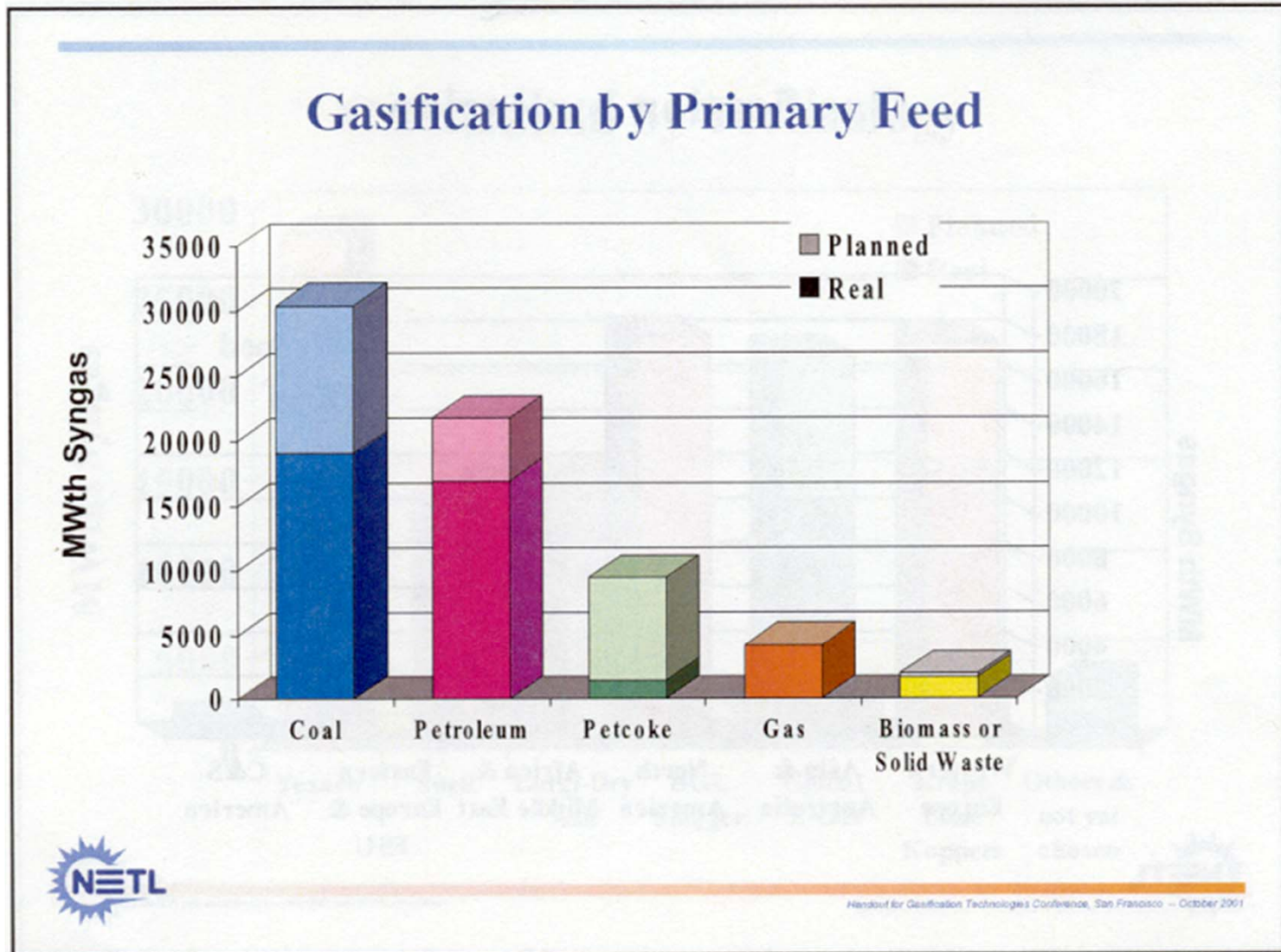
- , 가
- 0.5% , ash

## □

- CO/ chemical energy
-

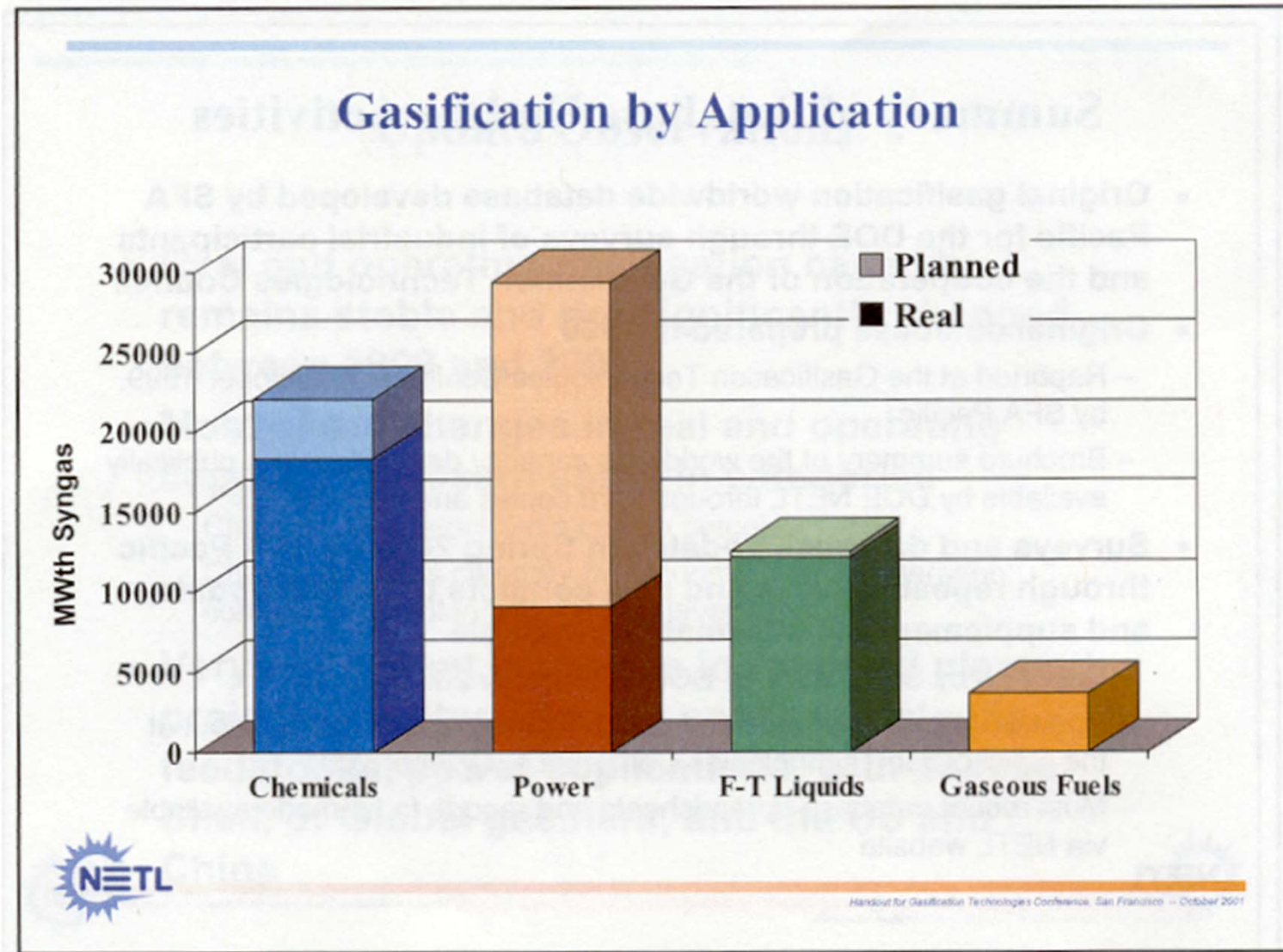
2001

# Gasification Syngas



2001

# Gasification Syngas



# DOE Vision 21

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## □ Goals:

- **Efficiency - Electricity Generation** (with no credit for cogeneration)
  - 60% HHV for coal-based systems
  - 75% LHV for NG-based systems
- **Efficiency - Combined Electricity/Heat**
  - Above 85% overall thermal efficiency
- **Efficiency - Fuels (H<sub>2</sub> or Liquid transportation fuel) only plant from coal**
  - 75% fuels utilization efficiency (LHV)
- **Environmental**
  - **Near zero emissions** : SO<sub>x</sub>, NO<sub>x</sub>, Particulates, Trace elements, Organic compounds
  - **40-50% CO<sub>2</sub> reduction**
  - 100% CO<sub>2</sub> reduction with sequestration
- **Costs**
  - Less than \$550/kW
- **Timing**
  - Improved gasifiers, Gas separation membranes begin by 2006
  - Designs for most subsystems, modules by 2012
  - **Commercial design by 2015**

# Vision 21 Program - 3 Areas

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## □ Enabling Technologies

- **Fuel-Flexible Gasification** : coal, coke, heavy-oil
- **Advanced Combustion Systems (PFBC, IFC)** :
  - recommended should not be included
- **Advanced Fuels & Chemicals** : Focusing reducing CO<sub>2</sub>
- **Fuel Cells**: - Focus on reducing Fuel Cell capital cost in large-scale, coal-gasification, central station power plants.
  - Distributed power generation FC program should not be in Vision 21
- **Fuel-Flexible G/T** : Focus on cycles using H<sub>2</sub> rather than Syngas

## □ Supporting Technologies & Systems Integration

- **Advanced Modeling & Systems Integration**
- **Materials & Heat Exchangers** : High temperature membranes for air separation, H<sub>2</sub> separation from syngas, High temperature coatings & materials
- **Environmental Control Technologies**
- **Gas Stream Purification**
- **Gas-Separation Technology**
- **Hydrogen Production from Water Dissociation**

## □ Commercialization

# Driving Force for Gasification

## □ Gasification is alive and growing

- 5,000 MW<sub>th</sub> syngas 가 (10%/yr)
- '99 4,000 MW<sub>th</sub>/yr 가

## □ project

## Coal & Petroleum coke

- pet coke 가

## □ IGCC

## deregulation

- 가 가 가 가 가 .
- Polygeneration 가 efficiency, revenue options, annual load가 가



# Future of Gasification

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- ❑ Continuing convergence of oil, gas & electric power markets with deregulation improves the potential for gasification.
- ❑ Gasification is helped by increasing interest in :
  - Clean alternatives to Natural Gas from low cost & stable supply fuels
  - Reduced emissions: SO<sub>2</sub>, NO<sub>x</sub>, PM<sub>2.5</sub>, Hg, solid/liquid wastes & CO<sub>2</sub>
  - Higher value-added pitch, pet coke & industrial waste utilization
- ❑ Electric power generation is the key market for gasification
  - Growing at a rate twice that of other end-use energy, like liquid fuels
  - Key to polygeneration is power to the grid for economy of scale.
  - GCC (Gasification Combined Cycle) repowering of existing coal units could have many advantages
  - GCC can be lower cost than NGCC at prices >\$4 per million Btu.





# Gasification

## □ Dongting Coal Gasification Project :

- Coal gasification : 2,000 /
- Syngas : 142,000 Nm<sup>3</sup>/hr (CO + H<sub>2</sub>), 3.4 million Nm<sup>3</sup>/day
- Syngas → Shift , Gas treatment → NH<sub>3</sub> → Urea plant
- Capital investment : 150 million US\$
- 50/50 Sinopec/Shell equity sharing : Gas treatment plant Sinopec 100%
- Ready-for-start-up : 2004

## □ Yingcheng Coal Gasification Project :

- Coal gasification : 910 /
- Syngas : 55,000 Nm<sup>3</sup>/hr (CO + H<sub>2</sub>)
- Chemical
- Plant owner : Hubei Shuanghuan Chemical Industrial Co., Ltd.
- Ready-for-start-up : 2004

## □ Other projects :

- Sinopec/Shell: Hubei Anqing 2,000 / → 3.4 million  
Nm<sup>3</sup>/day Chemical 가 2005 startup

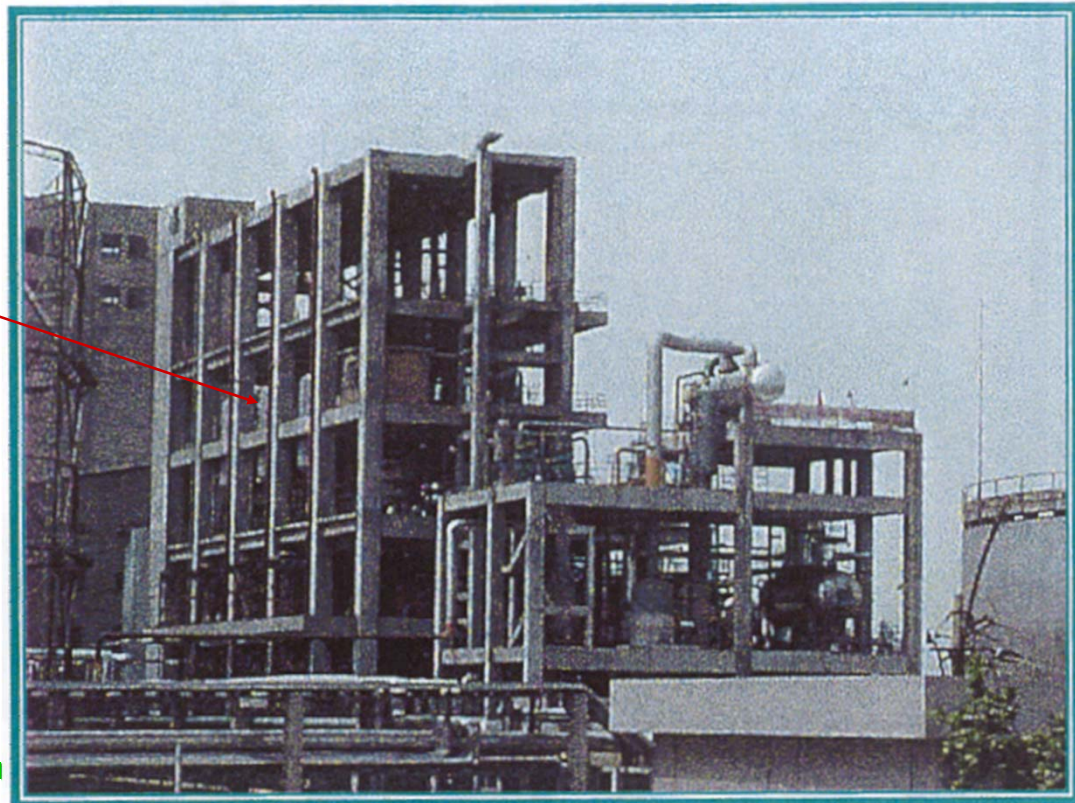
# Gasification

( )

## □ Huainan Coal Gasification Plant

- Coal gasification : 990 /
- Syngas → Urea
- Texaco ( ChevronTexaco)
- Start-up : 2000 8

3 Gasification trains



# IGCC



- 2007 , 2013 , 2014  
30 kW Clean Coal Technology(CCT)
- 2001 3 , CCT IGCC, PFBC IGCC KOPEC
- , .



## LG-Caltex / SK Corp.

- 30-60 kW IGCC .
- ,  
IGCC가 LG-Caltex



**2005**

**NOx**

**80 ppm**

- : NOx 150 ppm

# IGCC

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## □ IGCC

- 
- 
- Emission Credit Trading :  
/

## □

- Demo Plant

## □

- 2-20 / IGCC 가
- 가
- Plant Plant Dynamic Simulation  
computer simulation
- spin-off
- - , Biomass 가
- ( : , )

# Wabash River IGCC Plant 2001 Gas Island Downtime Causes

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Downtime Cause	% of Year	Corrective Action
Syngas Cooler tube leak	5.82	Limit dp & thermal cycles
Acid Gas Cooler tube leak	3.40	Proper refractory anchors
Slurry Mixer replacement	0.40	Min. flow constraints
Slurry flow interruption	0.72	Improved suction nozzle & operating discipline
False filter pressure indication	0.12	Simplified sensing lines & smarter control code
Miscellaneous	0.11	Actions implemented

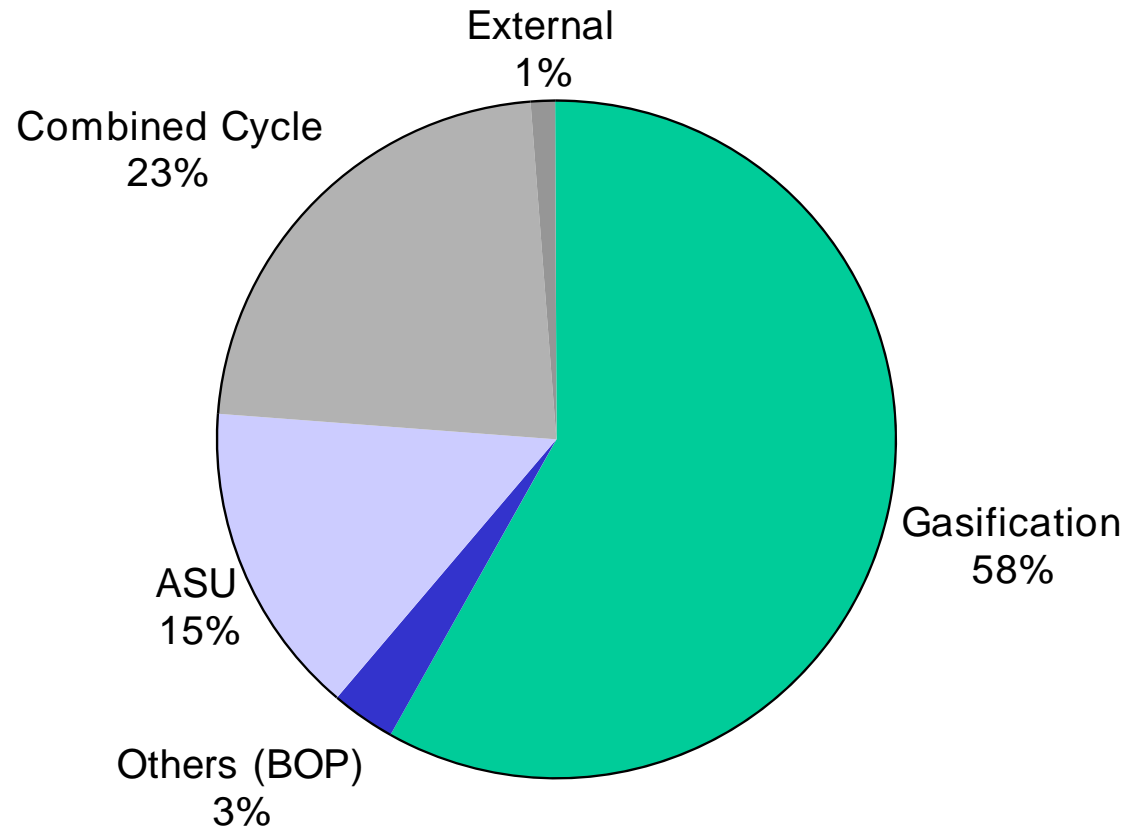
**Key Areas** : Hot gas cooling tube , feeding,

# Wabash River IGCC Plant 2001 Reliability by Gasification Sub-System

Sub-System	Reliability	Sub-System	Reliability
1st Stage Gasifier	99.5%	Acid Gas Removal	100%
2 <sup>nd</sup> Stage Gasifier	100%	Sulfur Recovery	96.6%
Raw Syngas Conditioning	100%	Sour Water Treatment	100%
Syngas Cooling	94.2%	Fuel Hopper System	100%
Particulate Removal	99.9%	Rod Mill System	100%
Chloride Scrubbing	100%	Slurry Storage System	99.9%
COS Hydrolysis	100%	Slurry Feed System	99.4%
Low Temp. Heat Recovery	100%	Slag Removal System	100%
Syngas Moisturization	100%	Cooling Tower System	100%

Reliability =  $[1 - (\text{Forced Outage Hours} / \text{Period Hours})] \times 100$   
: Scheduled shutdown period

# 335 MWe급 스페인 Puertollano IGCC Plant 분야별 문제점 - IGCC Trip (Area별) -



IGCC  
(Air Separation Unit)

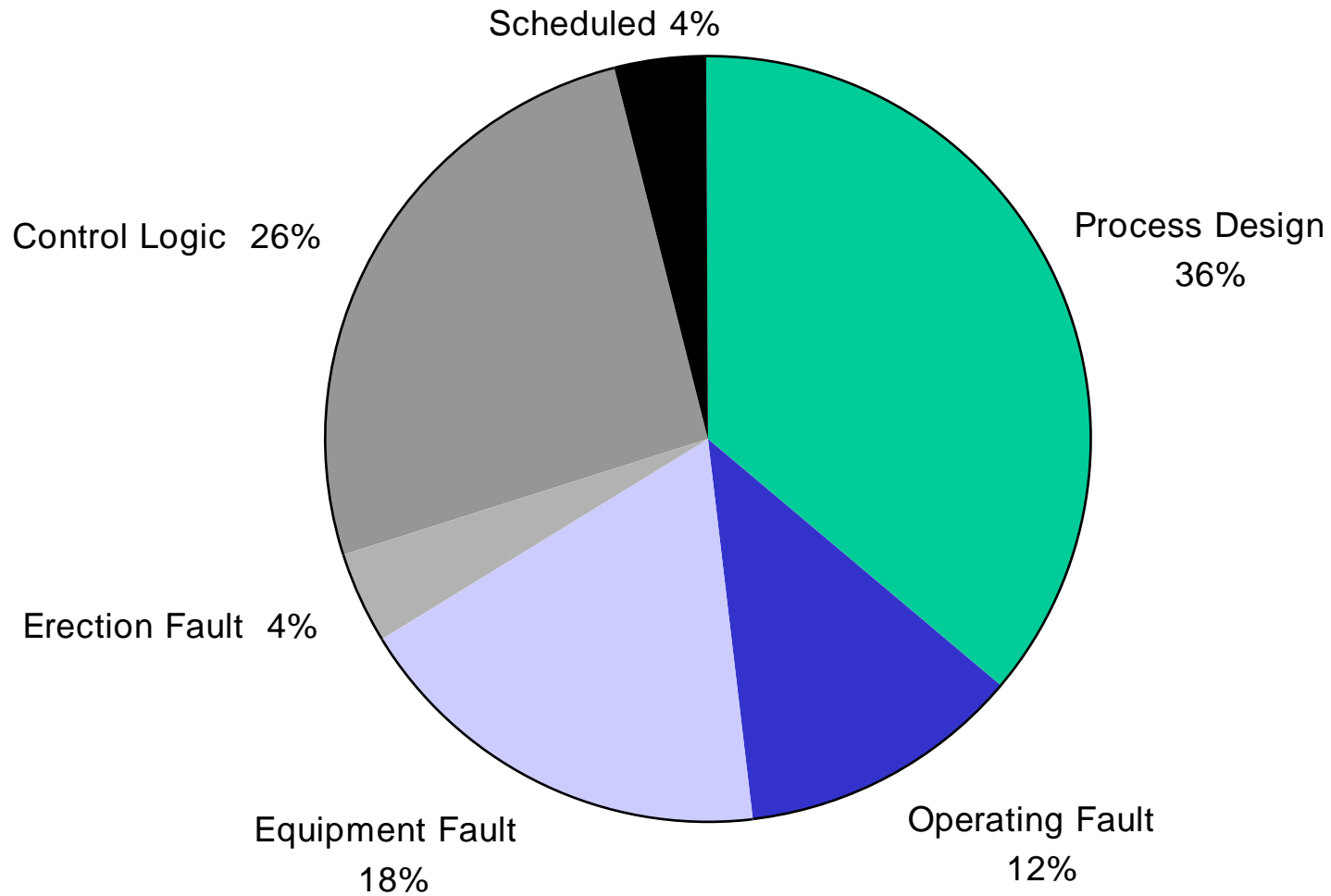
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# Puertollano IGCC

- IGCC Trip (Failure Type별) -

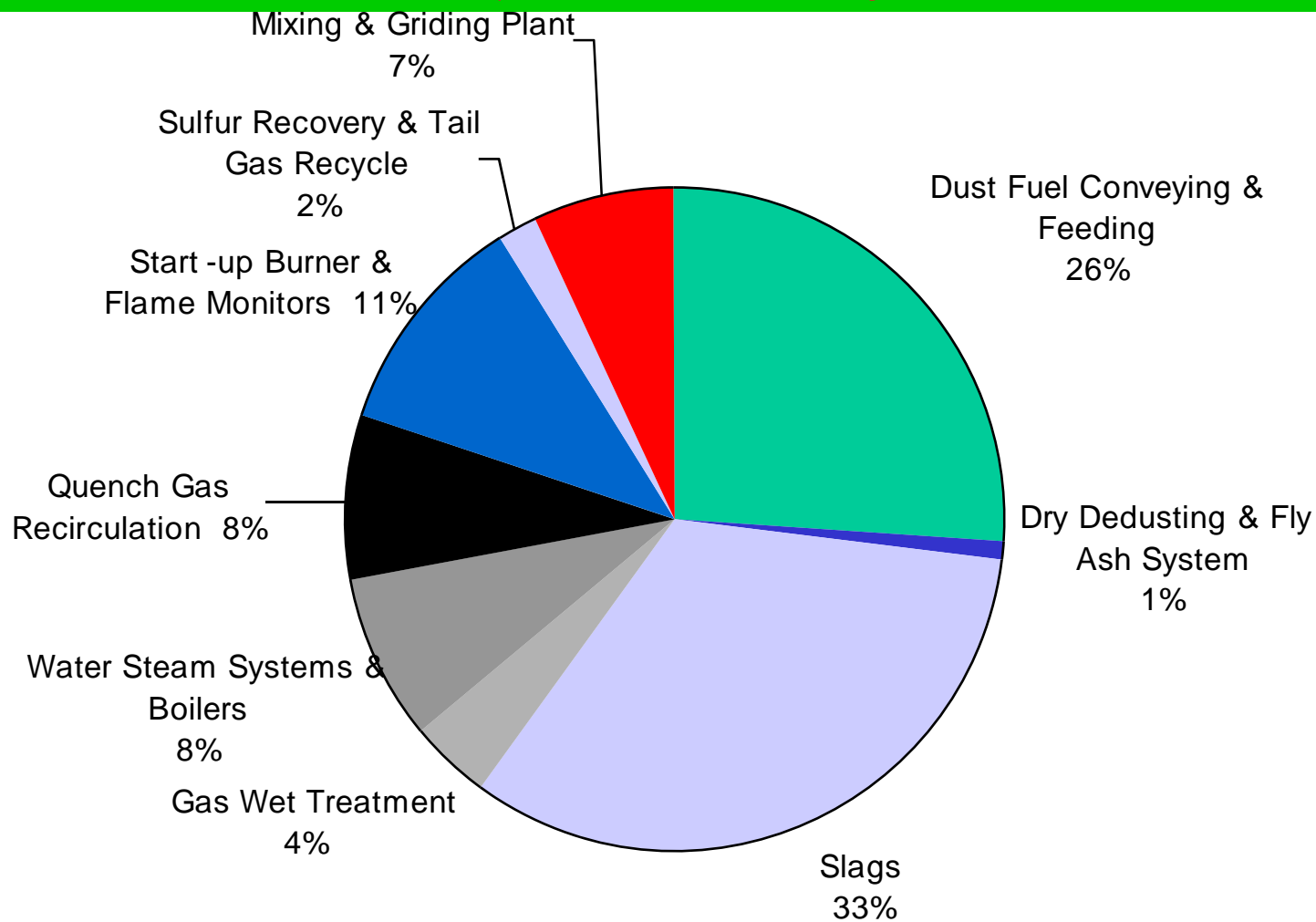


IGCC 가 가 .



# Puertollano IGCC

## - IGCC Trip (Gasification System별) -



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## Coal Feed to Gasification - RD&D Needs



- Coal Pump
- Coal/Water slurry heating. Better atomization and vaporization
- Lock hopper systems problematic at HP
- New concepts using slurry pumping to achieve HP
  - Slurry flash with cyclone underflow to gasifier and flashed steam added to raw gas for shift
  - Evaporate slurry with gasifier raw gas, cyclone and filter catch fed to gasifier. (See BI-GAS, HRL IDGCC and van der Burgt/KEMA/EPRI OGCC).
- Coal in liquid CO<sub>2</sub> slurries either directly or with flash evaporation (EPRI/ADL): water quench for shift etc.
- Re-examine above concepts for IGCC with shift and CO<sub>2</sub> removal and particularly for low cost low rank coals.

EPRI

IAE

Ref.: N. Holt, 2001 Gasification Tech. Conf.

# Entrained Flow Gasifiers RD&D Needs



Candidate Improved Design Features

Improvement/Technology	Shell/Prenflo	Texaco	Global E-Gas	Mitsubishi	Noell/GSP
HP Dry Feed System	✓	✓	✓	✓	✓
Add 2nd Stage	✓	✓			✓
Reduce Gas Recycle	✓				
Partial Quench	✓	✓	✓	✓	✓
Fire Tube SGC	✓	✓		✓	✓
Continuous Slag Removal	✓	✓		✓	✓
High Pressure	✓		✓	✓	✓
Other		New Radiant SGC	Cylindrical Design	Use O <sub>2</sub>	

EPRI



Ref.: N. Holt, 2001 Gasification Tech. Conf.

# Entrained Gasifier Design RD&D Needs

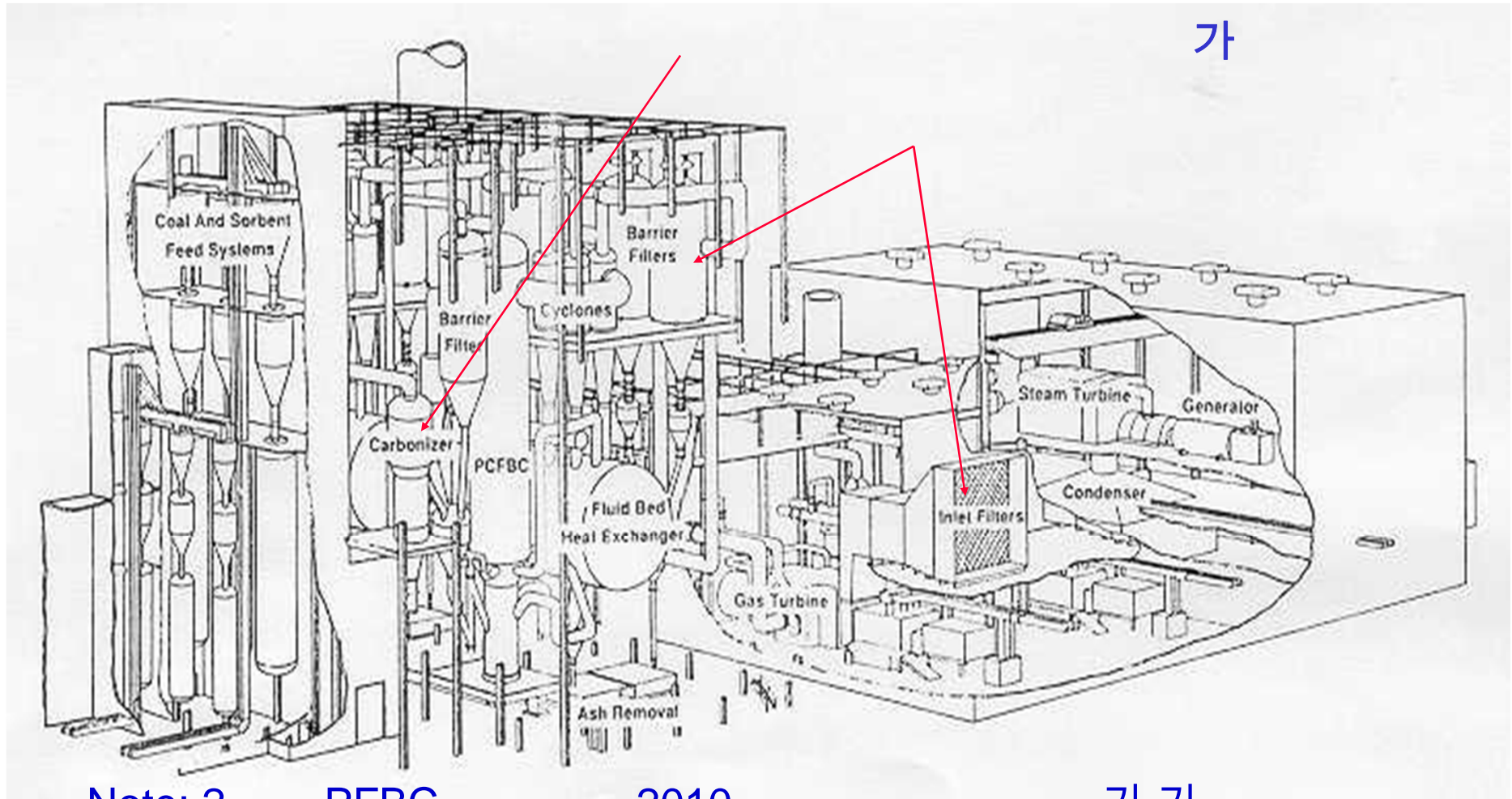


- Actual reaction rates not known and size based on pilot experience.
- Slurry reactors need additional time to evaporate water.
- Reaction rate varies inversely with coal rank.
- Petroleum coke reactivity < most bituminous coals.
- Accords with experience e.g. Ube petroleum coke.
- Scale up Montebello → Ruhrchemie → Cool water satisfactory for bituminous coals. However at Tampa, lower carbon conversion per pass experienced for both Pittsburgh #8 and Illinois #6 coals, than at Cool water.
- Co-gasification of coal and petroleum coke may have advantages for petroleum coke carbon conversion.

EPRI

IAE

Ref.: N. Holt, 2001 Gasification Tech. Conf.



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Note: 2

PFBC

2010

가 가

가

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PFBC

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□ IGCC 가  
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( : 가 ) 가 ,  
3 , ) 가 .

□ 가  
가 .  
□ 가 , biomass,  
( : ) 가  
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□ IGCC 가  
1/1000 ,  
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IGCC 가 .