

Model for Mixed-Electrolyte,
Aqueous Mixed-Solvent Systems
(Ind. Eng. Chem. Res. 1996)

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Introduction

- Debye- Hückel
 - for dilute electrolyte solution
- Pitzer (1973)
 - Single salt aqueous system
- Bromley (1973)
 - 2 ionic constants for each ion
 - 1 salt parameter, extend to mixed- electrolyte

Introduction

➤ Meissner (1972)

- 1 salt parameter, extended to mixed-electrolyte
- extrapolated to high concentration

➤ Chen, Evans (1986)

- NRTL term + D-H term ; nonidealities
- 2 parameters

Introduction

➤ Gibbs function

- D-H term + short range interaction term
- NRTL : Cruz and Renon (1978)
Chen et al (1982), Mock et al (1986)
- UNIFAC : Kikic et al (1991)
Achard et al (1994)
- UNIQUAC : Polka et al (1994), Li et al (1994)
Macedo et al (1990), Sandler (1986)

Introduction

- Different models for solute and solvent
- In this work,
 - unified model for mixed solute and mixed solvent system
 - : short range : electrostatic interaction ,
non-electrostatic interaction

Excess Gibbs Function Model

➤ D-H term

$$G_{DH}^{E*} = - \frac{RTV}{4\pi a^3 N_a} \left[\ln(1 + aK) - aK + \frac{(aK)^2}{2} \right]$$

○ by De M. Cardoso and O'Connell (1987)

$$\ln \gamma_{DH,j} = \frac{\bar{V}_j}{4\pi a^3 N_a} \left[\ln(1 + aK) - \frac{aK}{2} - \frac{aK}{2(1 + aK)} \right] \quad \text{For Solvent}$$

$$\ln \gamma_{DH,\pm i}^* = - \frac{|z_{+i} z_{-i}|}{16\pi a^3 N_a I} \frac{(aK)^3}{(1 + aK)} \quad \text{For Solute}$$

Excess Gibbs Function Model

- Short-range interaction term
 - segment number , surface area parameter, nonelectrostatic interaction energy parameter
 - from Helmholtz function
 - new lattice-hole theory (Yoo et al 1995)
 - $A \cong G^E$ (Wong and Sandler, 1992)

Excess Gibbs Function Model

$$G^E = G_A^E + G_R^E$$

- athermal contribution in symmetric convention

$$\beta G^E = \sum N_i \ln \frac{\theta_i}{x_i} + \left(1 - \frac{z}{2}\right) \sum N_i q_i \ln \frac{q_M r_i}{r_M q_i}$$

- residual contribution of UNIQUAC

$$\beta G^E = -\frac{zN_q}{2} \sum \theta_i \ln \left(\sum \theta_j \tau_{ji} \right)$$

Excess Gibbs Function Model

➤ Solvent Activity coefficients

$$\ln \gamma_{A,j} = \ln \frac{\theta_j}{x_j} + r_j \left(1 - \frac{z}{2} \right) \ln \frac{q_M r_j}{r_M q_j}$$

$$\ln \gamma_{R,j} = \frac{z q_j}{2} \left\{ 1 - \ln \left(\sum \theta_k \tau_{kj} \right) - \sum_k \frac{\theta_k \tau_{jk}}{\sum_l \theta_l \tau_{lk}} \right\}$$

$$\ln \gamma_j = \ln \gamma_{DH,j} + \ln \gamma_{A,j} + \ln \gamma_{R,j}$$

Excess Gibbs Function Model

➤ osmotic coefficient : $\phi = -n_{sol} \ln x_i \gamma_i / \sum_k^{salt} \nu_{\pm k} n_k$

➤ solute activity coefficient

$$\ln \gamma_{A,\pm i}^* = \sum \frac{\nu_i}{\nu_{\pm}} \ln \frac{\theta_i x_i^{\infty}}{\theta_i^{\infty} x_i} + \left(1 - \frac{z}{2}\right) \left(\sum \frac{r_i \nu_i}{\nu_{\pm i}} \right) \ln \frac{q_M r_M^{\infty}}{q_M^{\infty} r_M}$$

$$\ln \gamma_{R,\pm i}^* = \frac{z}{2} \sum \frac{\nu_i q_i}{\nu_{\pm i}} \left\{ \ln \frac{\sum \theta_j \tau_{ji}}{\sum \theta_j^{\infty} \tau_{ji}} + \sum_l \frac{\theta_j \tau_{ij}}{\sum \theta_k \tau_{kj}} - \sum_l \frac{\theta_j^{\infty} \tau_{ij}}{\sum \theta_k^{\infty} \tau_{kj}} \right\}$$

Excess Gibbs Function Model

- Interaction between ions $\epsilon_{ij} = \epsilon_{ij}^{(e)} + \epsilon_{ij}^{(n)}$
- interaction with uncharged species $\epsilon_{ij} = \epsilon_{ij}^{(n)}$
 - nonelectrostatic interaction

$$\epsilon_{ij}^{(n)} = (\epsilon_{ii}^{(n)} \epsilon_{jj}^{(n)})^{1/2} (1 - k_{ij})$$

➤ Parameters : molecular (r_i, ϵ_{ii}),
ions ($r_i, \epsilon_{ii}, r_{s,+i}, r_{s,-i}$), k_{ij}
by Robinson and Stokes 1955 data

parameters

Single Electrolyte Aqueous Systems

Table 3. Summary of Root Mean Square Errors for Osmotic Coefficients in Single-Electrolyte Aqueous Systems

	max. I	σ %		max. I	σ %
HCl	6.0	2.26	CsOH	1.0	0.28
HBr	1.0	0.54	CsNO ₃	1.4	1.73
HI	3.0	0.73	Cs ₂ SO ₄	5.4	1.61
HClO ₄	6.0	3.90	NH ₄ Cl	6.0	0.73
HNO ₃	3.0	0.49	NH ₄ NO ₃	6.0	1.84
LiCl	6.0	3.18	(NH ₄) ₂ SO ₄	6.0	4.05
LiBr	6.0	4.51	MgCl ₂	6.0	2.94
LiI	3.0	1.74	MgBr ₂	6.0	2.62
LiClO ₄	4.0	1.08	MgI ₂	6.0	2.19
LiOH	4.0	1.03	Mg(ClO ₄) ₂	6.0	3.66
LiNO ₃	6.0	0.38	Mg(NO ₃) ₂	6.0	1.61
Li ₂ SO ₄	6.0	0.72	MgSO ₄	6.4	5.20
NaCl	6.0	1.46	CaCl ₂	6.0	1.44
NaBr	4.0	0.64	CaBr ₂	6.0	1.97
NaI	3.5	0.44	CaI ₂	6.0	3.26
NaClO ₄	6.0	3.95	Ca(ClO ₄) ₂	6.0	2.85
NaOH	6.0	4.34	Ca(NO ₃) ₂	6.0	5.01
NaNO ₃	6.0	2.08	SrCl ₂	6.0	1.47
Na ₂ SO ₄	6.0	2.08	SrBr ₂	6.0	2.17
KCl	4.8	0.46	SrI ₂	6.0	2.85
KBr	5.0	0.84	Sr(ClO ₄) ₂	6.0	3.37
KI	4.5	2.59	Sr(NO ₃) ₂	6.0	5.73
KOH	6.0	4.30	BaCl ₂	5.4	1.96
KNO ₃	3.5	0.85	BaBr ₂	6.0	1.64
K ₂ SO ₄	2.1	1.66	BaI ₂	6.0	1.73
CsCl	6.0	1.06	Ba(ClO ₄) ₂	6.0	5.46
CsBr	5.0	0.93	Ba(NO ₃) ₂	1.2	1.86
CsI	3.0	1.74	average		2.20

Mixed Electrolyte Aqueous System

Table 5. Summary of Root Mean Square Errors for Osmotic Coefficients in Mixed-Electrolyte Aqueous Systems

	max. f	σ %	ref		max. f	σ %	ref
NaCl-LiCl	6.0	2.66	a	MgCl ₂ -Mg(NO ₃) ₂	3.9	1.74	k
NaCl-LiCl	5.8	2.53	b	KCl-Na ₂ SO ₄	4.4	0.99	m
LiCl-BaCl ₂	4.3	2.73	c	LiCl-LiNO ₃	6.0	2.62	p
NaCl-CaCl ₂	5.3	1.46	d	KCl-NaBr	4.2	0.91	ti
CsCl-NaCl	6.0	1.83	e	Na ₂ SO ₄ -K ₂ SO ₄	3.6	1.12	m
NaCl-BaCl ₂	4.8	1.11	f	HClO ₄ -LiClO ₄	4.5	2.45	l
CsCl-BaCl ₂	4.1	1.51	g	LiClO ₄ -NaClO ₄	5.2	1.57	l
KCl-CaCl ₂	5.0	1.38	g	KCl-LiCl	5.0	4.18	q
KCl-BaCl ₂	4.7	2.08	f	NaCl-KNO ₃	3.7	0.68	j
NaCl-KCl	6.4	1.06	g	KCl-NaNO ₃	5.8	2.40	ti
CaCl ₂ -MgCl ₂	6.5	1.66	d	NaCl-KBr	4.5	1.49	l
NaCl-NaBr	4.3	1.19	i	MgCl ₂ -Ca(NO ₃) ₂	6.2	3.13	k
CsCl-KCl	5.0	1.72	a	Mg(NO ₃) ₂ -Ca(NO ₃) ₂	6.0	4.90	k
NaBr-KBr	4.3	1.07	j	Mg(NO ₃) ₂ -CaCl ₂	4.3	2.63	k
KCl-KBr	4.3	0.70	j	KCl-K ₂ SO ₄	2.1	2.73	m
NaCl-NaNO ₃	5.7	1.49	j	NaCl-Na ₂ SO ₄	2.5	0.86	m
KCl-KNO ₃	3.7	0.91	j	NaCl-K ₂ SO ₄	3.6	0.81	o
NaNO ₃ -KNO ₃	3.7	1.13	j	K ₂ SO ₄ -CaSO ₄	3.5	2.93	n
NaNO ₃ -LiNO ₃	6.3	2.92	b	Na ₂ SO ₄ -CaSO ₄	6.4	2.96	n
CaCl ₂ -Ca(NO ₃) ₂	5.9	3.85	k	Li ₂ SO ₄ -CaSO ₄	6.5	9.58	n
CsCl-LiCl	5.0	8.03	a	Li ₂ SO ₄ -Na ₂ SO ₄	6.2	2.24	v
HClO ₄ -NaClO ₄	5.4	2.52	i	Li ₂ SO ₄ -K ₂ SO ₄	5.1	4.44	w
HClO ₄ -NaClO ₄	6.1	3.11	f	average		2.34	

^a Robinson and Liro, 1953. ^b Robinson et al., 1971. ^c Lindenbaum et al., 1972. ^d Robinson and Bower, 1966b. ^e Robinson, 1952. ^f Robinson and Tower, 1965. ^g Robinson, 1961. ^h Robinson and Bower, 1966a. ⁱ Covington et al., 1968. ^j Debye et al., 1970. ^k Platford, 1971. ^l Rusi and Johnson, 1978. ^m Robinson et al., 1972. ⁿ Filippov et al., 1987. ^o Filippov et al., 1989.

Mixed Electrolyte Aqueous System

Table 8. Summary of Root Mean Square Errors in Solubilities of Comp(2) in the Presence of Comp(1) for Water-Methanol Mixed-Solvent Systems^a

Comp(1)	Comp(2)	methanol wt. fract.	max f	σ%		ref
				present	Pitzer	
NaCl	KCl	0.0	6.2	3.9	3.4	a
HCl	NaCl	0.0	6.4	14.7	4.0	a
HCl	KCl	0.0	6.4	4.0	7.3	a
NaOH	Na ₂ SO ₄ ·10H ₂ O	0.0	6.2	1.0	7.1	a
NaCl	CaSO ₄ ·2H ₂ O	0.0	3.1	19.2		a
CaCl ₂	CaSO ₄ ·2H ₂ O	0.0	3.2	28.1		a
Na ₂ SO ₄	CaSO ₄ ·2H ₂ O	0.0	5.4	13.4		a
NaCl	KCl	0.1	5.6	5.5		b
NaCl	KCl	0.2	4.1	5.1		b
NaCl	KCl	0.3	3.5	8.5		b
NaCl	KCl	0.4	2.7	3.5		b
NaCl	KCl	0.5	2.5	15.9		b
average				5.9	5.5	

^aLink and Seidel, 1965. ^bSham and Lee, 1991. ^cSolubility Product Values: NaCl (aq, 37.06), KCl (aq, 7.81), KCl (10% MeOH, 4.05), KCl (20% MeOH, 1.89), KCl (30% MeOH, 0.884), KCl (40% MeOH, 0.438), KCl (50% MeOH, 0.084), Na₂SO₄·10H₂O (aq, 0.052), Na₂SO₄ (aq, 0.28), CaSO₄·2H₂O (aq, 3.9 × 10⁻⁵)

Mixed Electrolyte Aqueous System

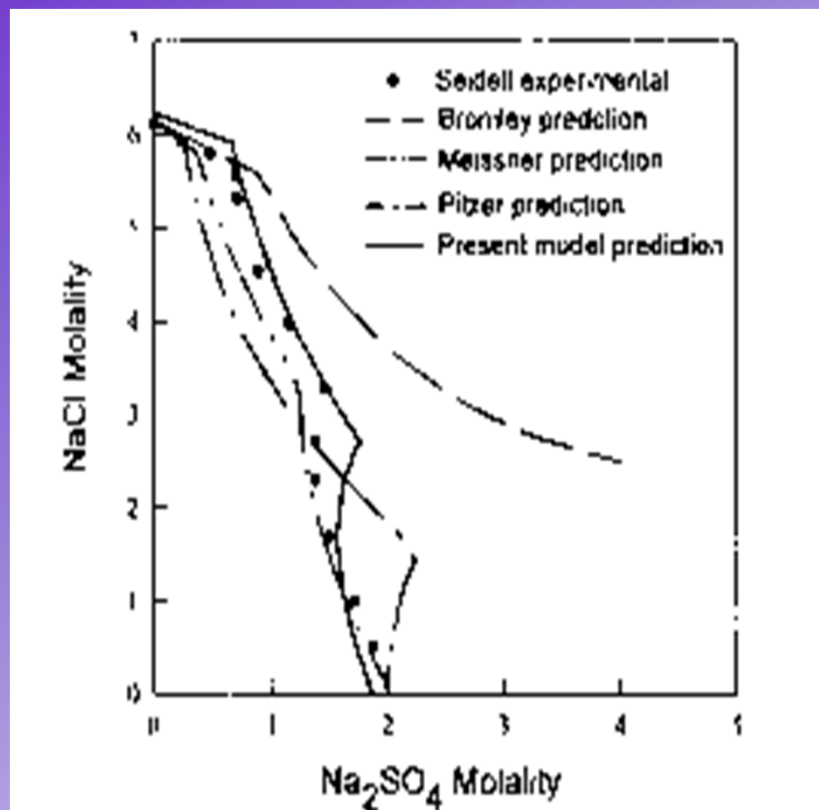


Figure 1. Comparison of solubilities for NaCl, Na₂SO₄, and Na₂SO₄·10H₂O in the H₂O-Na₂SO₄-NaCl system by various methods at 25 °C.

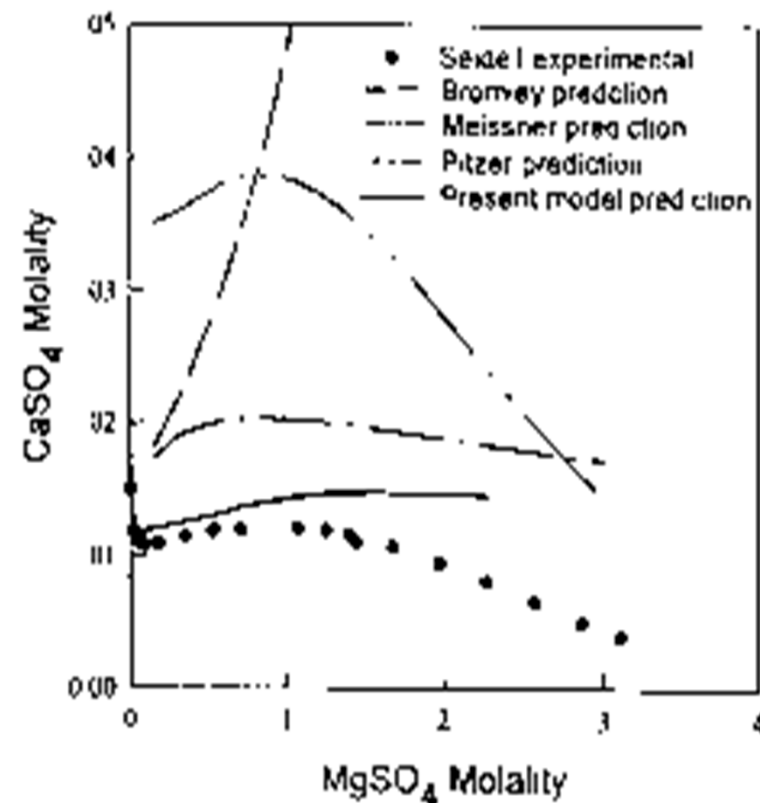


Figure 2. Comparison of solubilities for CaSO₄·2H₂O in the H₂O-MgSO₄-CaSO₄ system by various methods at 25 °C.

Conclusion

- A unified excess Gibbs function model for mixed-electrolyte mixed-solvent system
- Short range interaction term : new lattice-hole Helmholtz free energy
- 2 parameters for solvent, 3 parameters for each ionic species