

Electrolyte Solutions

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- Aqueous chemistry
 - introduction, definition
- Phase equilibrium
 - predictive model
- Thermodynamics
 - properties, data source, activity models

Aqueous chemistry (1)

- Aqueous electrolyte system
 - Aqueous-based environmental applications
 - gas treatment, waste water treatment (chromatographic separations, membrane separations, pH controlled neutralization) chemical waste disposal
 - Typical applications
 - bio separations, corrosion, oilfield research, geothermal wells, paper production
- Difficulties of phase equilibrium models
 - describing the nonideal behavior
 - mean activity coefficient
 - different standard state
 - complex chemistry

Aqueous chemistry (2)

- Aqueous systems terminology
 - Phase
 - physical state of chemical species. (g, l, aq, s)
 - Electrolyte
 - some solubility in water and reacts in water.
 - Nonelectrolyte
 - some solubility in water and remains nearly totally in the molecular form.
 - Ionic species
 - dissolved in water and possessing charge, cation or anion
 - Molecular species
 - dissolved in water and no charge
- Thermodynamics & Properties LAB
KOREA University*

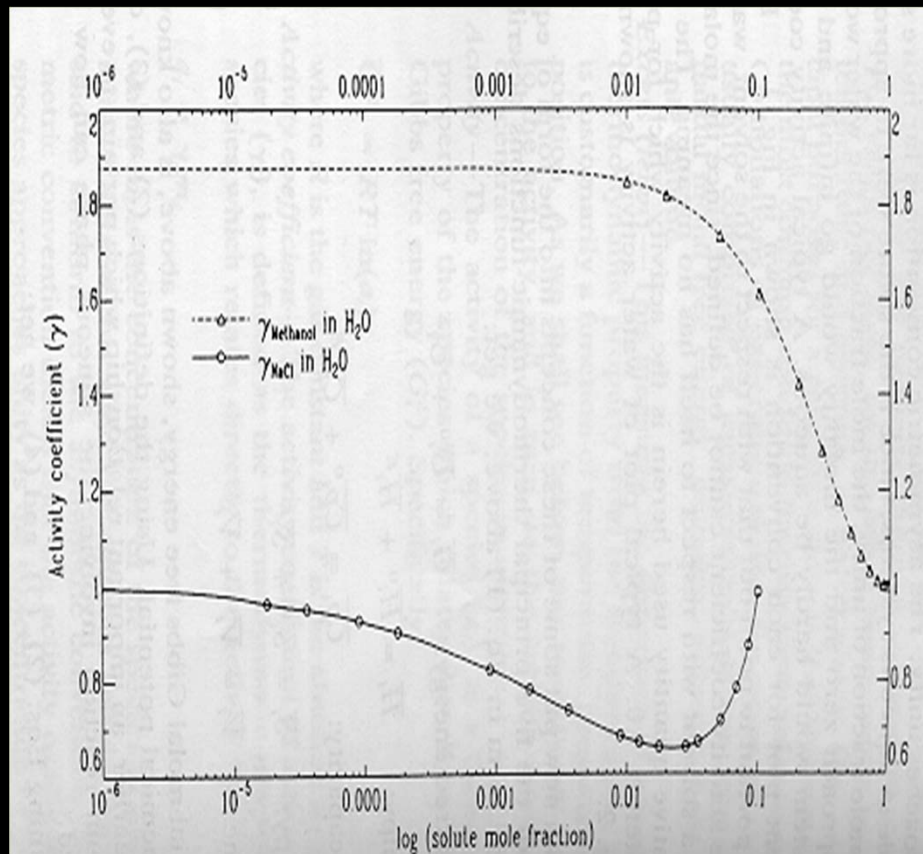
Aqueous Chemistry (3)

- **Complex, ion pair**
 - composed of both cationic and anionic portions, charged or uncharged
- **Strong electrolyte**
 - completely dissociates to base ions
- **Weak electrolyte**
 - partially dissociates
- **Aqueous electrolyte equilibrium**
 - thermodynamic equilibrium involving all species in the aqueous phase
- **Aqueous phase equilibrium**
 - thermodynamic description of physical equilibrium between aqueous phase and other phase.

- Aqueous Thermodynamic Definitions
 - Solvent
 - Solute - dissolved in water
 - Molality
 - moles of an aqueous phase species per kg of water
 - Thermodynamic properties - G, H, S, Cp, V
$$\overline{P}_i = \overline{P}_i^0 + \overline{P}_i^E$$
 - Standard state term - at defined state (c, T, P)
 - Reference state - at specific standard state

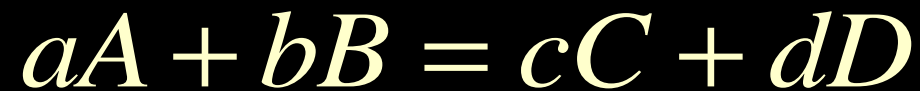
Aqueous Chemistry (5)

- Excess term - nonideal contributions, activity
 - Activity, Activity coefficient (symmetric, asymmetric)



- Equilibrium Constants

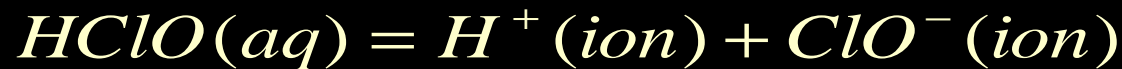
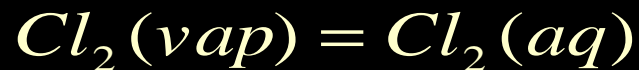
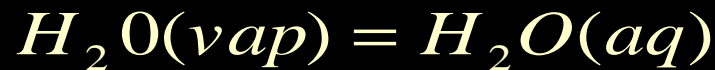
- equilibrium reaction



$$K = \frac{(\gamma_C m_C)^c (\gamma_D m_D)^d}{(\gamma_A m_A)^a (\gamma_B m_B)^b}$$
$$= \exp\left[-\overline{\Delta G_{rxn}}(T) / RT\right]$$

Phase equilibrium (1)

- Predictive model (water - chlorine system)



- Given : T, P, M^0 of H_2O, m^0 of Cl_2
- Calculate : $v, P_1, P_2, m_{HClO}, m_{Cl_2}, m_{H^+}, m_{OH^-}, m_{Cl^-}, m_{ClO^-}, m_{H_2O}(aq)$ - 10 unknowns.

Phase equilibrium (2)

- Equilibrium constant (5)
- Electroneutrality equation : cation = anion (1)

$$m_{H^+} = m_{Cl^-} + m_{OH^-} + m_{ClO^-}$$

- material balance (4)

$$3M_{H_2O}^0 + 2m_{Cl_2}^0 = 3M_{H_2O} + M_{H_2O} / 55.51(3m_{HClO} + m_{Cl^-} + 2m_{OH^-} + m_{H^+} + 2m_{Cl_2(aq)}) + v$$

$$2m_{Cl_2}^0 = M_{H_2O} / 55.51(m_{HClO} + m_{Cl^-} + m_{ClO^-}) + vP_2 / P$$

$$2M_{H_2O}^0 = 2M_{H_2O} + M_{H_2O} / 55.51(m_{HClO} + m_{H^+} + m_{OH^-}) + vP_1 / P$$

$$P = P_1 + P_2$$

- Representation of the thermodynamic properties

$$P_T = \sum_i^n \bar{P}_i N_i$$

- thermodynamic consistency
- Gibbs free energy
 - activity coefficient

$$\bar{S}_i = - \left(\frac{\partial \bar{G}_i}{\partial T} \right)_{P,m}$$

$$\bar{H}_i = \bar{G}_i + T \bar{S}_i$$

$$\bar{C}_{pi} = \left(\frac{\partial \bar{H}_i}{\partial T} \right)_{P,m}$$

$$\bar{V}_i = \left(\frac{\partial \bar{G}_i}{\partial P} \right)_{T,m}$$

- Sources of Data
 - Compilations of G, H, S, Cp
 - Chase et al.(1985) : ref. state (s, l, g)
 - Cox et al.(1989) : ref. state (s, l, g, aq)
 - Daubert and Danner (1989) : ref. T dependent
 - Glushko et al. (1965-1981) : ref. (aq), NBS
 - Kelly (1960) : ref. state H, Cp, S (s)
 - Compilations of Equilibrium Constants
 - Baes and Mesmer (1976) : hydrolysis equilibria for metal cations
 - Smith and Martell (1975-1989) : complexation equilibria for anions, organic anions

- Compilations of Activity Coefficient Data
 - Goldberg (1981) : univalent and bivalent electrolytes
 - Goldberg and Nutall (1978) : alkalin metals
 - Hammer and Wo (1972) : univalent electrolytes
 - Lobo (1989) : activity coefficient data , viscosity, transport, density, osmotic coefficient data

- Compilations of Solubility data
 - Horvath(1982) : halogenated hydrocarbons
 - Linke and Seidell (1958, 1965) : inorganic compounds
 - Stephen and Stephen (1963) : organic compounds

- Standard State Properties $\overline{G}_i^0, \overline{H}_i^0, \overline{S}_i^0, \overline{C}_{pi}^0, \overline{V}_i^0$

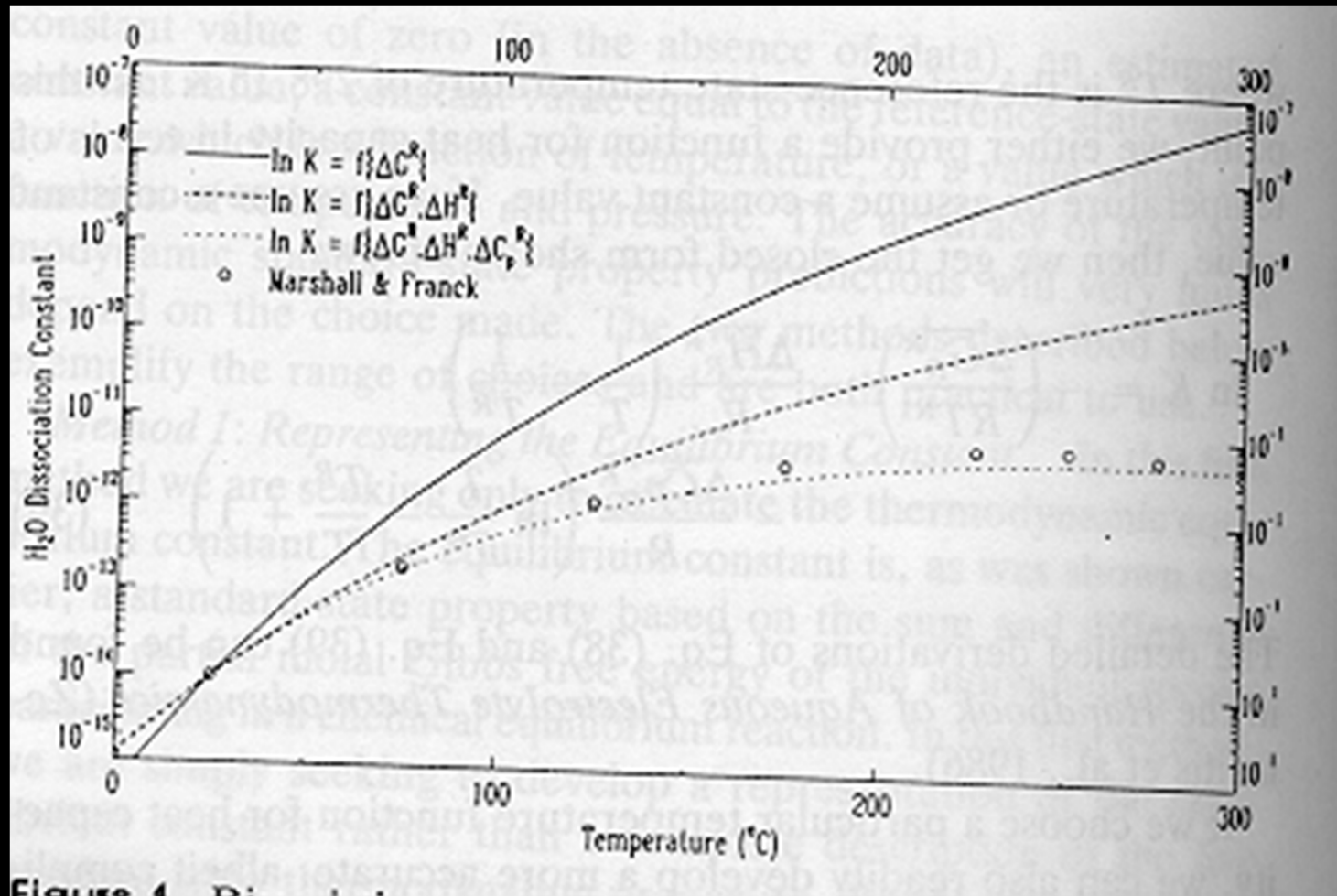
- Representing the Equilibrium Constant

$$\ln K = -\left(\frac{\overline{\Delta G}_{Rxn}^R}{RT^R}\right) - \frac{\overline{\Delta H}_{Rxn}^R}{R} \left(\frac{1}{T} - \frac{1}{T^R}\right) - \frac{\overline{\Delta C}_p^R}{R} \left(\ln \frac{T}{T^R} - \frac{T^R}{T} + 1\right)$$

- Helgeson Equation of State :

$\overline{\omega}, c1, c2, a1, a2, a3, a4$ - 7 coefficients

Thermodynamics(5)



Thermodynamics(6)

Table 1 Standard State Thermodynamic Values Using the Helgeson Equation of State

$$\bar{V}^0 = a_1 + a_2 \left(\frac{1}{\psi + P} \right) + \left[a_3 + a_4 \left(\frac{1}{\psi + P} \right) \right] \left(\frac{1}{T - \theta} \right)$$

$$- \omega Q + \left(\frac{1}{\epsilon} - 1 \right) \left(\frac{\partial \omega}{\partial P} \right)_T$$

$$\bar{C}_P^0 = c_1 + c_2 \left(\frac{1}{T - \theta} \right)^2 - \left(\frac{2T}{T - \theta} \right)^3$$

$$\times \left[a_3(P - P_r) + a_4 \ln \left(\frac{\psi + P}{\psi + P_r} \right) \right] + \omega TX$$

$$+ 2TY \left(\frac{\partial \omega}{\partial T} \right)_P - T \left(\frac{1}{\epsilon} - 1 \right) \left(\frac{\partial^2 \omega}{\partial T^2} \right)_P$$

$$\bar{S}^0 = \bar{S}_{P_r, T_r}^0 + c_1 \ln \left(\frac{T}{T_r} \right) - \frac{c_2}{\theta} \left\{ \left(\frac{1}{T - \theta} \right) - \left(\frac{1}{T_r - \theta} \right) \right\}$$

$$+ \frac{1}{\theta} \ln \left[\frac{T_r(T - \theta)}{T(T_r - \theta)} \right]$$

$$+ \left(\frac{1}{T - \theta} \right)^2 \left[a_3(P - P_r) + a_4 \ln \left(\frac{\psi + P}{\psi + P_r} \right) \right]$$

$$+ \omega Y - \left(\frac{1}{\epsilon} - 1 \right) \left(\frac{\partial \omega}{\partial T} \right)_P - \omega_{P_r, T_r} Y_{P_r, T_r}$$

where

ϵ = dielectric constant of the solvent (for our studies the solvent is water)

ψ = a constant term in pressure (= 2600 bar)

θ = a constant term in temperature (= 228 K)

ω = Born term in temperature and pressure (Tanger, 1986)

$$Y = \frac{1}{\epsilon^2} \left(\frac{\partial \epsilon}{\partial T} \right)_P$$

where P is the pressure (in bar) and T is the temperature (in kelvins)

$$X = \left(\frac{\partial Y}{\partial T} \right)_P$$

$$Q = \frac{1}{\epsilon^2} \left(\frac{\partial \epsilon}{\partial P} \right)_T$$

Table 1 Continued

$$\Delta \bar{H}_{P, T} = \Delta \bar{H}_f^0 + c_1(T - T_r) - c_2 \left[\left(\frac{1}{T - \theta} \right) - \left(\frac{1}{T_r - \theta} \right) \right]$$

$$+ a_1(P - P_r) + a_2 \ln \left(\frac{\psi + P}{\psi + P_r} \right) + \left(a_3(P - P_r) \right)$$

$$+ a_4 \ln \left[\frac{\psi + P}{\psi + P_r} \right] \left[\frac{2T - \theta}{(T - \theta)^2} \right] + \omega \left(\frac{1}{\epsilon} - 1 \right)$$

$$+ \omega TY - T \left(\frac{1}{\epsilon} - 1 \right) \left(\frac{\partial \omega}{\partial T} \right)_P - \omega_{P_r, T_r} \left(\frac{1}{\epsilon_{P_r, T_r}} - 1 \right)$$

$$- \omega_{P_r, T_r} T_r Y_{P_r, T_r}$$

$$\Delta \bar{G}_{P, T}^0 = \Delta \bar{G}_f^0 - \bar{S}_{P_r, T_r}^0(T - T_r) - c_1 \left[T \ln \left(\frac{T}{T_r} \right) - T + T_r \right]$$

$$+ a_1(P - P_r) + a_2 \ln \left(\frac{\psi + P}{\psi + P_r} \right)$$

$$+ \left[a_3(P - P_r) + a_4 \ln \left(\frac{\psi + P}{\psi + P_r} \right) \right] \left(\frac{1}{T - \theta} \right)$$

$$- c_2 \left[\left(\left(\frac{1}{T - \theta} \right) - \left(\frac{1}{T_r - \theta} \right) \right) \right]$$

$$\left(\frac{\theta - T}{\theta} \right) - \frac{T}{\theta^2} \ln \left(\frac{T_r(T - \theta)}{T(T_r - \theta)} \right) \right]$$

$$+ \omega \left(\frac{1}{\epsilon} - 1 \right) - \omega_{P_r, T_r} \left(\frac{1}{\epsilon_{P_r, T_r}} - 1 \right) + \omega_{P_r, T_r} Y_{P_r, T_r} (T - T_r)$$

- Excess Properties

- Ionic strength

$$I = \frac{1}{2} \sum_{i=1}^{nI} z_i^2 m_i$$

- activity coefficient

- long range term : dilute solutions

- Debye and Hückel term or modified D-H

- short range term : concentrated solution

- ion-ion, ion-molecule interaction

- mean activity coefficient

$$\gamma_{\pm} = (\gamma_+^x \gamma_-^y)^{1/(x+y)}$$

- History of activity coefficient models
 - Debye-Hückel model
 - Guggenheim's equation : one parameter
 - Davies' equation
 - Bromley's equation
 - Meissner's equation : reduced activity coefficients
 - Pitzer's equation : 3~4 parameters model
 - Helgeson : EoS approach
 - Chen's equation : short and long range interactions using two parameters

- Debye-Hückel (1920') : from electric potential

$$\log \gamma_{\pm} = \frac{-A|z_+z_-|\sqrt{I}}{(1 + a_0B\sqrt{I})} + CI$$

- Guggenheim's (1935)

$$\log \gamma_{c,a} = -\frac{\alpha|z_+z_-|\sqrt{I}}{1 + \sqrt{I}} + \frac{2v_+}{v_+ + v_-} \sum_{a'} \beta_{c,a'} m_{a'} + \frac{2v_-}{v_+ + v_-} \sum_{c'} \beta_{c',a} m_{c'}$$

- Davies's (1938)

$$\log \gamma_{\pm} = \frac{A|z_+z_-|\sqrt{I}}{1 + \sqrt{I}} + Bm$$

- Bromley's (1972)

$$\log \gamma_{\pm} = -\frac{A|z_+z_-|\sqrt{I}}{1 + \rho\sqrt{I}} + \frac{(B_0 - B)I}{(1 + aI^2)} + BI + CI^2$$

- Meissner's (1978) : reduced activity coefficients

$$\Gamma^o = \{1 + B(1 + 0.1I)^q - B\}\Gamma^* \quad \Gamma^o = \gamma_{\pm}^{1/z_+z_-}$$

- Pitzer (1973~1978)

$$\ln \gamma_{\pm} = |z_+z_-|f^{\pm} + m \left(\frac{2\nu_+\nu_-}{\nu} \right) B_{\pm}^{\gamma} + m^2 \left[\frac{2(\nu_+\nu_-)^{1.5}}{\nu} \right] C_{\pm}^{\gamma}$$

- Helgeson (1981)
- Chen (1982)
 - NRTL method, long range and short range contribution

$$\ln f_{\pm} = \ln f_{\pm}^P + \ln f_{\pm}^{lc}$$

- Temperature effect

Thermodynamics(13)

