

# 1. Theory for Pure-liquid Surface Tension

## I ) Brock and Bird Method (HC\_SRFBROCK)

Brock and Bird proposed the following relation for nonpolar liquids.

$$\frac{\mathbf{s}}{P_c^{2/3} T_c^{1/3}} = (0.132 \mathbf{a}_c - 0.279)(1 - T_r)^{11/9} \quad (1)$$

Using the relation by Miller Eq. (1) is derived as ;

$$\mathbf{s} = P_c^{2/3} T_c^{1/3} Q(1 - T_r)^{11/9} \quad (2)$$

$$Q = 0.1196 \left[ 1 + \frac{T_{br} \ln(P_c / 1.01325)}{1 - T_{br}} \right] - 0.279 \quad (3)$$

where surface tension,  $\mathbf{s}$  is in dyne/cm, and temperature and pressure are in Kelvins and bars, respectively.

### References :

Brock, J. R., and R. B. Bird, *AIChE J.*, **1**, 174, 1955

Miller, D. G., *Ind. Eng. Chem. Fundam.*, **2**, 78, 1963

Poling et al., "Properties of Gases and Liquids", 5<sup>th</sup> ed. McGraw-Hill, New York

## II ) Zuo and Stenby Method (HC\_SRFZUO)

Zuo and Stenby proposed the two-reference fluid corresponding-state approach such as the following relation.

$$\mathbf{s}_r = \ln \left( 1 + \frac{\mathbf{s}}{T_c^{1/3} P_c^{2/3}} \right) \quad (4)$$

The units in Eq. (4) are bar, kelvins, and dyn/cm. In this method,  $\mathbf{s}_r$  for the fluid of interest is related to  $\mathbf{s}_r$  for two reference fluid which are methane (1) and n-octane (2) and related by the following expression.

$$\mathbf{s}_r = \mathbf{s}_r^{(1)} + \frac{\mathbf{w} - \mathbf{w}^{(1)}}{\mathbf{w}^{(2)} - \mathbf{w}^{(1)}} (\mathbf{s}_r^{(2)} - \mathbf{s}_r^{(1)}) \quad (5)$$

For methane,

$$\mathbf{s}^{(1)} = 40.520(1 - T_r)^{1.287} \quad (6)$$

and for n-octane

$$\mathbf{s}^{(2)} = 52.095(1 - T_r)^{1.21548} \quad (7)$$

### References :

Zuo, Y.-X., and E. H. Stenby, *Can. J. Chem. Eng.*, **75**, 1130,

Poling et al., "Properties of Gases and Liquids", 5<sup>th</sup> ed. McGraw-Hill, New York

**Notice :** Method (I) and (II) are not satisfactory for polar fluid. For polar fluids, the following method is recommended.

### III ) Sastri and Rao Method (HC\_SRF SR)

Sastri and Rao proposed the following equation to treat the components with strong hydrogen-bonding.

$$S = KP_c^x T_b^y T_c^z \left[ \frac{1-T_r}{1-T_{br}} \right]^m \quad (8)$$

The units in Eq. (8) are kelvins and bars. Parameters for Eq. (8) are show in Table 1 for each class of components.

Table 1. Values of Constants for Sastri-Rao Method, Eq. (8)

	<i>K</i>	<i>x</i>	<i>y</i>	<i>z</i>	<i>m</i>
Alcohols	2.28	0.25	0.175	0	0.8
Acids	0.125	0.50	-1.5	1.85	11/9
All others	0.158	0.50	-1.5	1.85	11/9

#### References :

Sastri, S. R. S., and K. K. Rao, *Chem. Eng. J.*, **59**, 181, 1995

Poling et al., "Properties of Gases and Liquids", 5<sup>th</sup> ed. McGraw-Hill, New York

## 2. KDB Routines for Pure-liquid Surface Tension Calculation

KDB pure-liquid surface tension calculation subroutines contain three estimation methods, which Brock-Bird method, Zuo-Stenby method, and Sastri-Rao method.

Subroutine Name	Description	Required Common Blocks
HC_SRFBROCK	Brock-Bird method	HC_PROP
HC_SRFZUO	Zuo-Stenby method	HC_PROP
HC_SRF SR	Sastri-Rao method for polar liquid	HC_NAME, HC_PROP

### I ) HC\_SRFBROCK

1. USAGE : CALL HC\_SRFBROCK(ICN,T,SRF,IST)

#### 2. ARGUMENTS

ICN : COMPONENT NUMBER (1-50) TO CALCULATE SURFACE TENSION  
(INTEGER, INPUT)

T : TEMPERATURE IN KELVIN (REAL\*8, INPUT)

SRF : SURFACE TENSION IN dyn/cm (REAL\*8, OUTPUT)

IST : STATUS OF CALCULATION (INTEGER, OUTPUT)

= 0 : NORMAL TERMINATION

= 911 : CRITICAL TEMPERATURE DATA NOT AVAILABLE

= 912 : CRITICAL PRESSURE DATA NOT AVAILABLE

- = 913 : NORMAL BOILING POINT DATA NOT AVAILABLE
- = 914 : GIVEN T EXCEEDS CRITICAL TEMPERATURE

### 3. Required properties

Critical temperature in K, critical pressure in kPa, and normal boiling point in K

## II ) HC\_SRFZUO

1. USAGE : CALL HC\_SRFZUO(ICN,T,SRF,IST)

### 2. ARGUMENTS

- ICN : COMPONENT NUMBER (1-50) TO CALCULATE SURFACE TENSION  
(INTEGER, INPUT)
- T : TEMPERATURE IN KELVIN (REAL\*8, INPUT)
  
- SRF : SURFACE TENSION IN dyn/cm (REAL\*8, OUTPUT)
- IST : STATUS OF CALCULATION (INTEGER, OUTPUT)
  - = 0 : NORMAL TERMINATION
  - = 921 : CRITICAL TEMPERATURE DATA NOT AVAILABLE
  - = 922 : CRITICAL PRESSURE DATA NOT AVAILABLE
  - = 923 : ACENTRIC FACTOR DATA NOT AVAILABLE
  - = 924 : GIVEN T EXCEEDS CRITICAL TEMPERATURE

### 3. Required Properties

Critical temperature in K, critical pressure in kPa., and acentric factor

## III ) HC\_SRF SR

1. USAGE : HC\_SRF SR(ICN,T,SRF,IST)

### 2. ARGUMENTS

- ICN : COMPONENT NUMBER (1-50) TO CALCULATE SURFACE TENSION  
(INTEGER, INPUT)
- T : TEMPERATURE IN KELVIN (REAL\*8, INPUT)
  
- SRF : SURFACE TENSION IN dyn/cm (REAL\*8, OUTPUT)
- IST : STATUS OF CALCULATION (INTEGER, OUTPUT)
  - = 0 : NORMAL TERMINATION
  - = 931 : CRITICAL TEMPERATURE DATA NOT AVAILABLE
  - = 932 : CRITICAL PRESSURE DATA NOT AVAILABLE

= 933 : NORMAL BOILING POINT DATA NOT AVAILABLE

= 934 : GIVEN T EXCEEDS CRITICAL TEMPERATURE

### 3. Required Properties

Critical temperature in K, critical pressure in kPa, and normal boiling point in K  
ICLASS(ICN) must be specified according to Table 1 for each component.