

Chapter 12 Fire and Explosion Hazards of Fine Powders

12.1 Introduction

Explosion

- Flammable gas: fuel concentration, local heat transfer conditions, oxygen concentration, initial temperature
- Dusts: + particle size distribution, moisture content

* Powders - High surface area / small size (small heat capacity)

Combustible powders → can be explosible

e.g. agricultural/chemical/coal/foodstuffs/metals/
pharmaceuticals/plastics/woodworking

- Organic dust :

heating → emission of combustible gases → explosion

- Metals :

protective oxide films → breaking by sudden heating

12.2 Combustion Fundamentals

(1) Flames

- Flammable materials + oxygen + ignition source
- Stationary flame vs. explosion flame
according to the behavior of flame front

(2) Explosion and Detonation

- Generation of gaseous combustion products
 - rapid gas expansion or
 - rapid pressure increase
- Detonation vs. deflagration

Determined by flame speed (< or > speed of sound) which is

governed by heat of combustion
 degree of turbulence
 ignition energy

* Primary vs. secondary explosion

↓

compression wave of small explosion → increase in resuspending particles

∴ Compression wave precedes the flame.

(3) Ignition - Simple Analysis for Ignition

Energy balance for fuel-air mixture:

$$\begin{aligned}
 & Q_{input} + (-\Delta H) \left[Z \exp\left(-\frac{E}{RT}\right) \right] C \rho_{m, fuel} = \\
 & \text{Heat input} \qquad \qquad \text{Heat generated} \\
 & V [C \rho_{m, fuel} C_{p, fuel} + (1 - C) \rho_{m, air} C_{p, air}] \frac{dT}{dt} + hA(T - T_s), \text{ J/s} \\
 & \qquad \qquad \qquad \qquad \qquad \text{heat accumulation} \qquad \text{heat dissipated}
 \end{aligned}$$

where C : volumetric concentration of fuel

ρ : molar density

V : volume of fuel-and-air mixture element

A : surface area of the element

* Figure 12.1

$T_B \rightarrow$ Ignition temperature

Explosion \rightarrow "Runaway" reaction

Figure 12.2 Effect of heat input

Figure 12.3 Autoignition(spontaneous ignition)

(4) Flammability Limits

- Upper and lower flammability limit, C_{fL} , C_{fU}
in volume % fuel
- Minimum oxygen for combustion

For C_3H_8 $C_{fL} = 2.2\%$ by volume,

$$MOC = C_{fL} \cdot \left[\frac{\text{moles } O_2}{\text{moles fuel}} \right]_{\text{Stoich}}$$

$$= 2.2 \cdot 5 = 11\% \text{ } O_2 \text{ by volume}$$

Worked Example 12.1

Worked Example 12.2

12.3 Combustion in Dust Clouds

(1) Fundamental to Specific to Dust Cloud Explosion

$$(-\Delta H) \left[Z \exp \left(-\frac{E}{RT} \right) \right] C_{p,m,fuel}$$

$$(-\Delta H)rV \quad \rightarrow \quad (-\Delta H)r'S \cdot \left(\frac{\text{surface fuel}}{\text{volume fuel}} \right) = (-\Delta H)r'S \cdot \frac{6}{x}$$

* Particle size : very important

- Dispersion
- Surface area for reaction
- Specific heat of reaction
- Heat up rate

(2) Characteristics of Dust Explosion

little data on powder properties

- Minimum dust concentration
- Minimum oxygen for combustion (MOC)
- Minimum ignition temperature
- Minimum ignition energy
- Maximum explosion pressure

- *Maximum rate of pressure rise*

$$\left(\frac{dp}{dt}\right)_{\max} V^{1/3} = K_{ST}$$

As close as possible to plant conditions

Table 12.1

Table 11.2 - Explosion class (K_{ST})

(3) Apparatus for Determination of Dust Explosion Characteristics

- Ignition source
- Dust dispersion
- Vertical tube apparatus Figure 12.4
(max. dust concentration, min. energy for ignition, MOC)
- Sphere apparatus Figure 12.5
(max. explosion pressure and max. rate of pressure rise)
- Godbert-Greenwald furnace apparatus (min. ignition temperature)

12.4 Control of the Hazard

(1) Introduction

- Change the process to eliminate the dust
- Design the plant to withstand the pressure generated by any explosion
- Remove the oxygen to below MOC
- Add moisture to the dust
- Add diluent powder to the dust

(2) Ignition Sources

Flames / Smouldering / hot surfaces / welding and cutting /
friction and impact / electric spark / spontaneous heating

(3) Venting

- Simple and inexpensive method

Figure 12.6

Worked Example 12.3

(4) Suppression

- Discharging a quantity of inert gas and inert powder into the vessel

* Suppression systems

Automatic venting/advance inerting/automatic shutdown

(5) Inerting

- N₂ and CO₂
- Oxygen concentration < MOC

(6) Minimize Dust Cloud Formation

- Use of dense phase conveying
- Use cyclone and filters instead of settling vessels
- Do not allow the powder stream to fall freely through the air

(7) Containment