

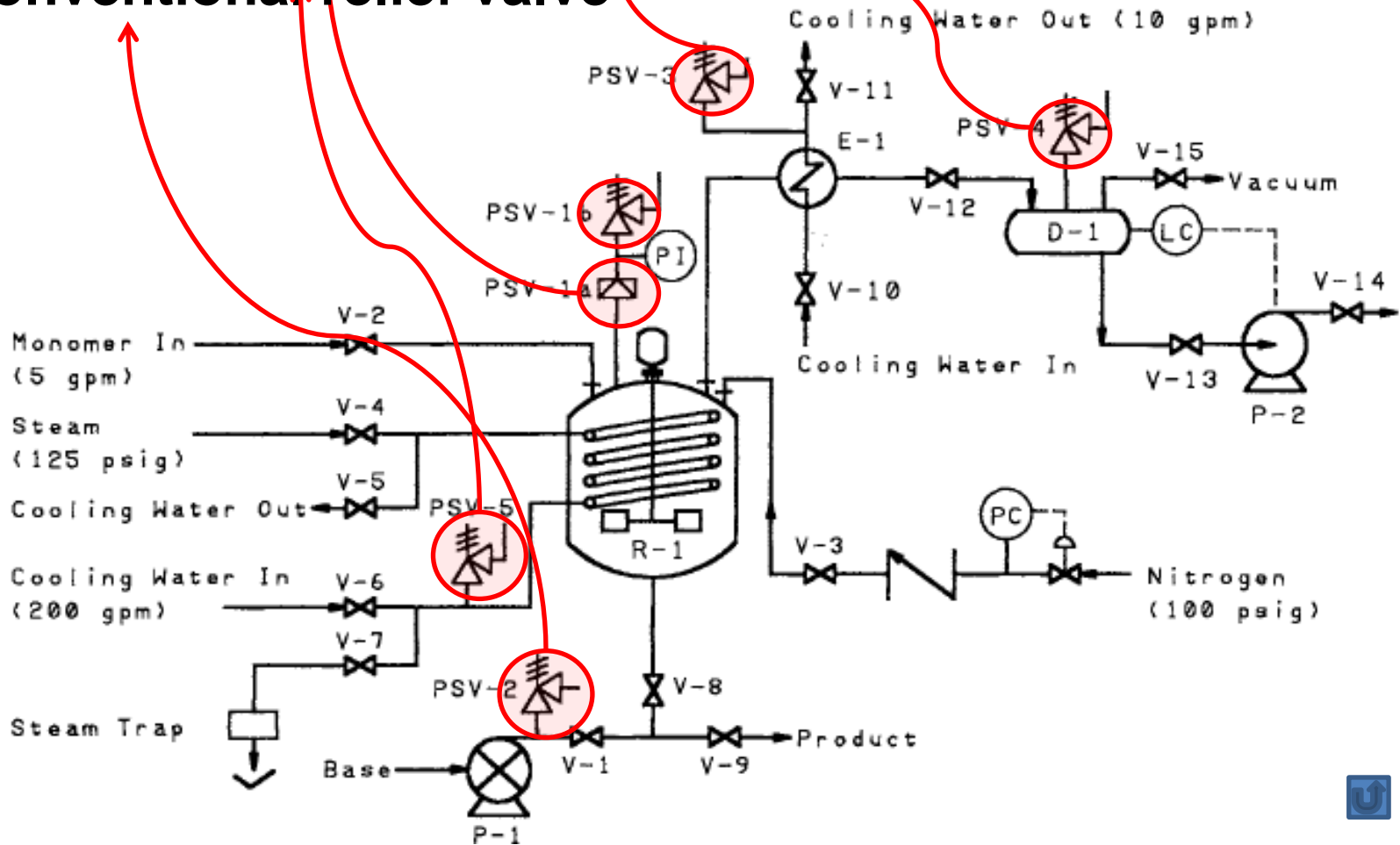
Relief Systems

Relief Scenarios

- **A single relief event requires a particulate vent area and valve size**
- **Relief scenarios are determined based on a PHA**
- **For each scenario, a vent area is calculated**
- **The worst-case scenario requires the largest vent area.**
- **Ex. Relief scenarios: Ex. 8-2, p. 363, Tab 8-2, p. 365**



A rupture disk to protect RSV-1b from the reactive monomers (plugging from polymerization) **conventional relief valve** a relief valve for liquid service only



Ex 8-2 Relief Scenarios



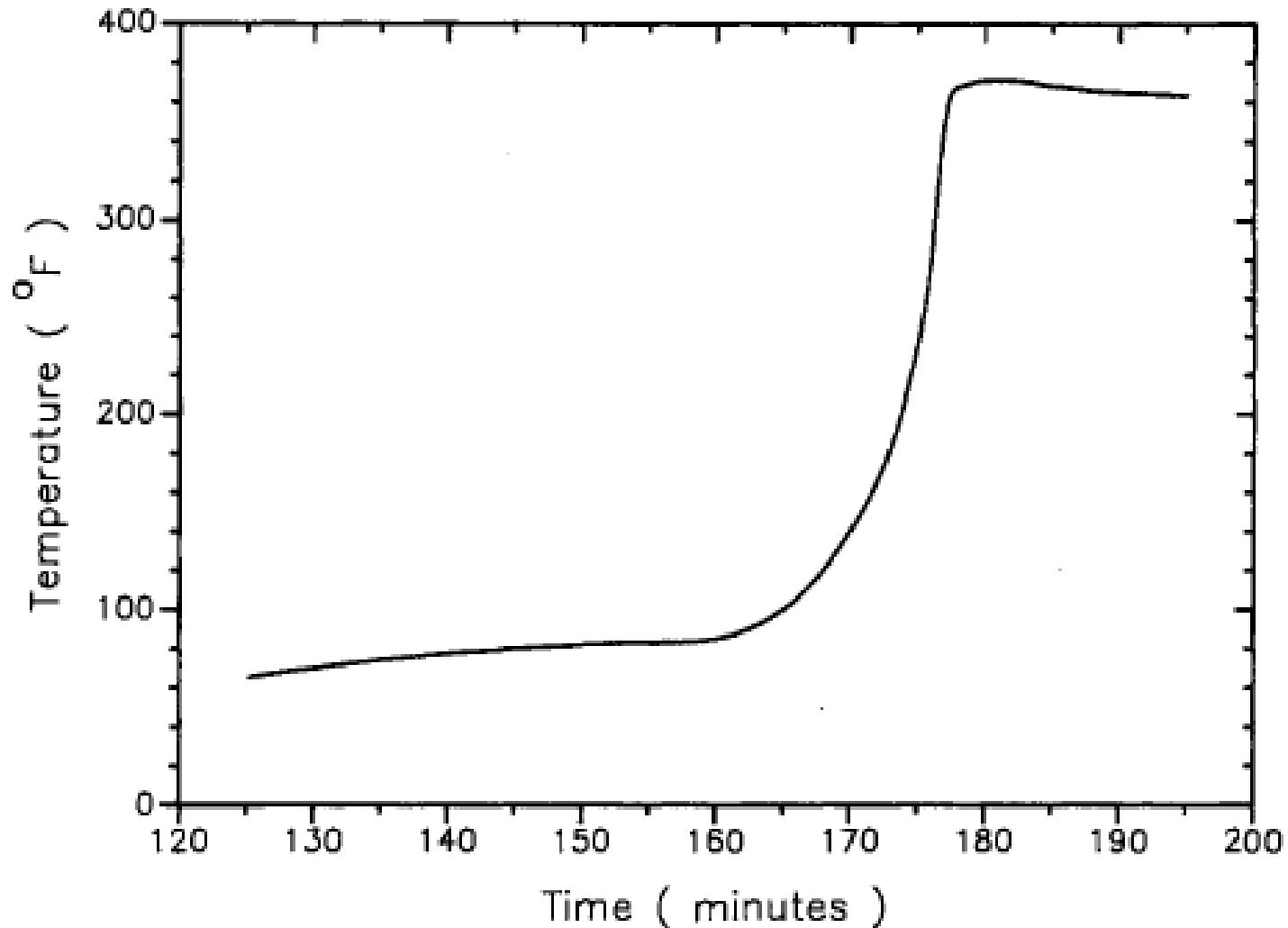
Relief Identifications	Scenarios
PSV-1a & PSV-1b	Vessel full of <i>l</i> and P-1 is accidentally actuated
	Cooling coil is broken and water enters at 200gpm and 50 psig
	N ₂ regulator fails, giving critical flow in 1" line
	Runaway rxn (Loss of cooling)
PSV-2	V1 is accidentally closed; systems need relief for 100 gpm at 50 psig
PSV-3	Confined water line is heated with 125-psig steam
PSV-4	N ₂ regulator fails, giving critical flow in 1/2" line
	The other R-1 scenario will be relieved via PSV-1
PSV-5	Water blocked inside coil, and heat of rxn causes thermal expansion

Data for Relief Sizing

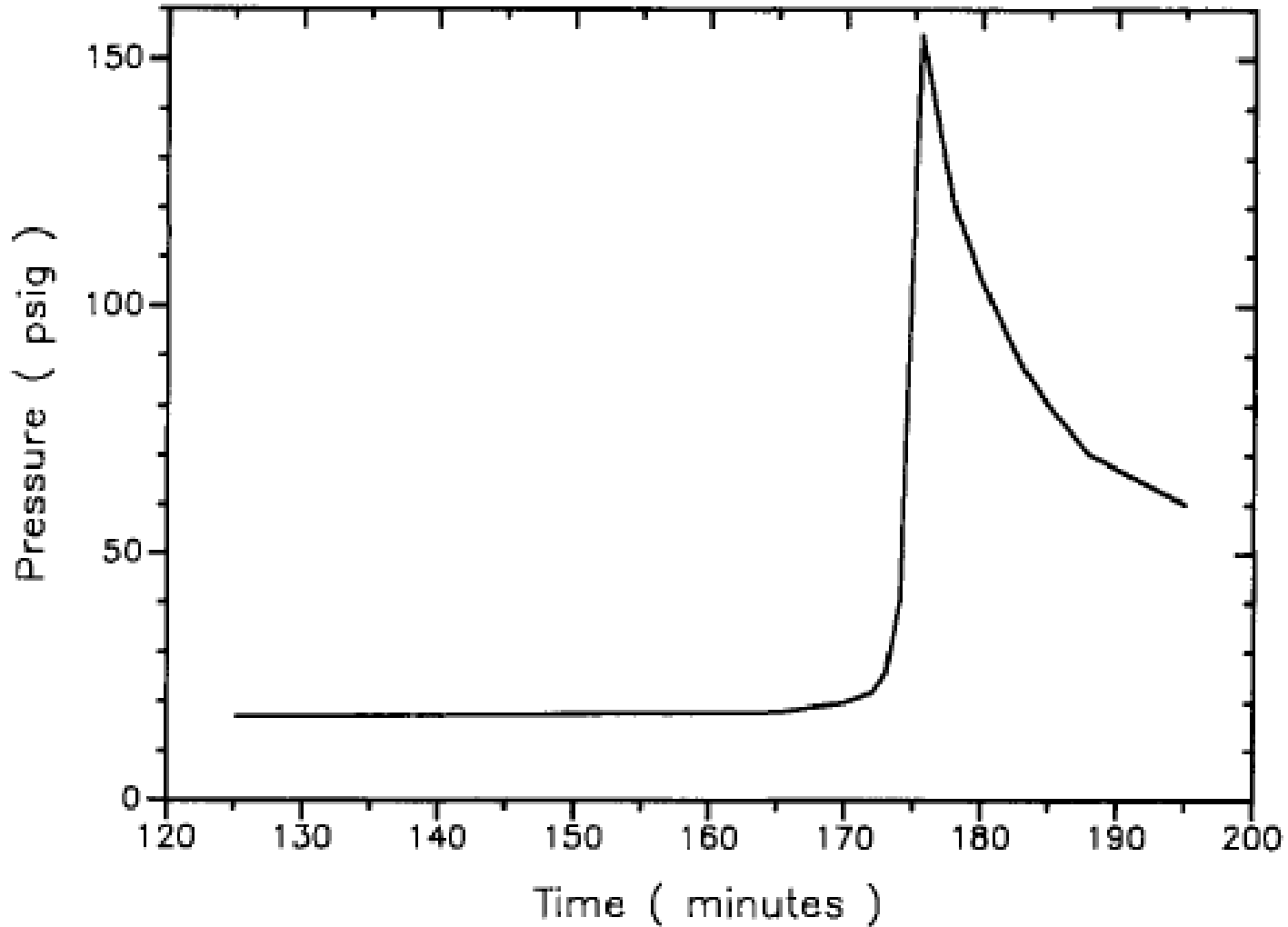
- **Physical property data**
- **Chemical reaction rate behavior**
- **Single phase releases: vapor, liquid, solid**
- **Multiple phase releases**
- **Runaway reaction relief: liquid & vapor**
- **Gas or dust explosions from combustion apparatus**
- **These data are part of the process safety information needed for a PHA**

Reaction Behavior Measurement

- **For accurate relief vent area determinations, experimental data are most important**
- **Calorimeters are used to characterize behavior during normal reaction or runaway.**
- **Sample is progressively heated to search for an exothermic reaction**
- **Raw data includes T, P, time, amount of non condensable gas formed, onset temperature, maximum heat rate, maximum pressure rate**

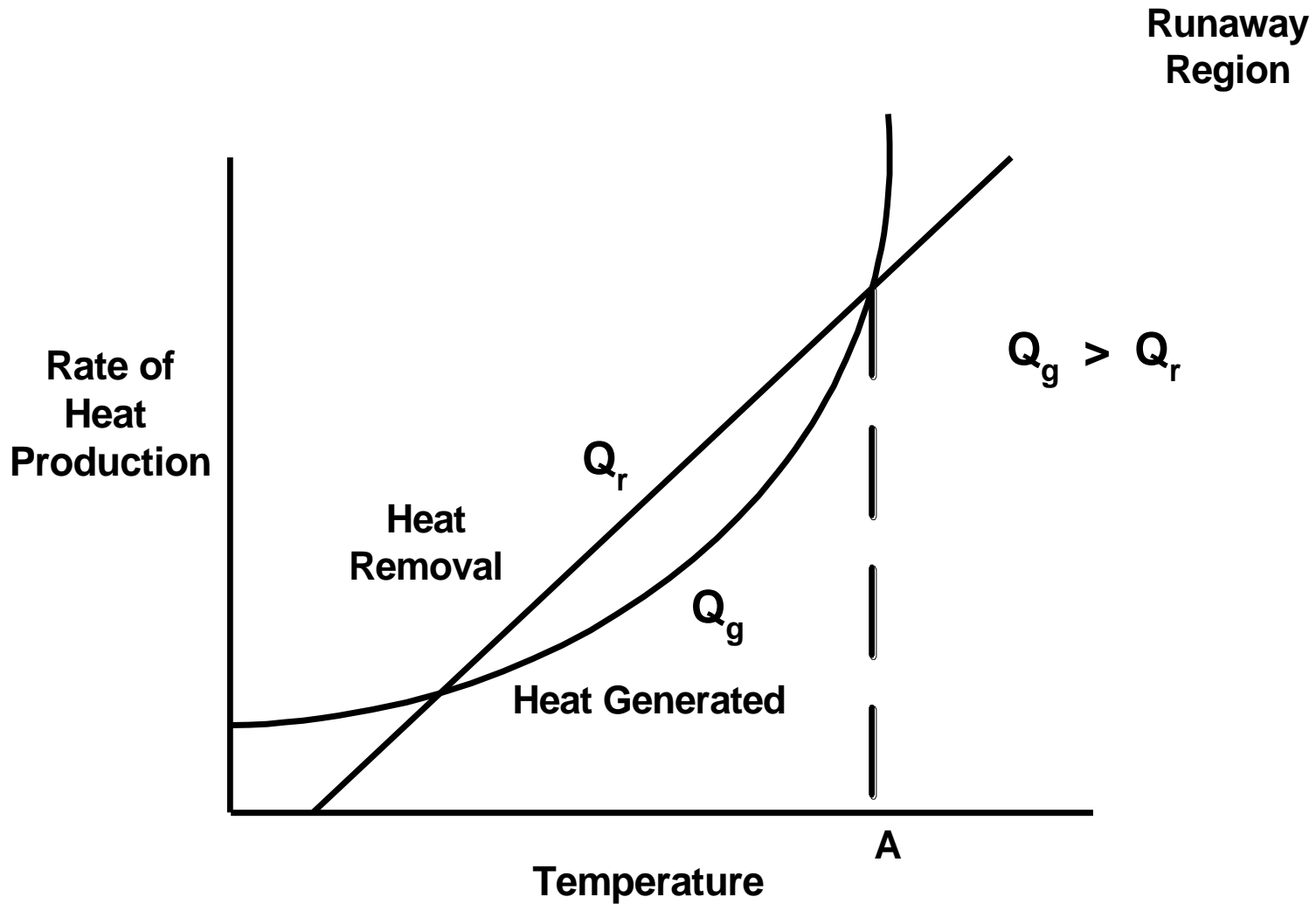


Runaway reaction temperature data acquired using the vent sizing package (VSP)



Runaway reaction pressure data acquired using the vent sizing package

Runaway Reaction Behavior



Preventing a Runaway Reaction

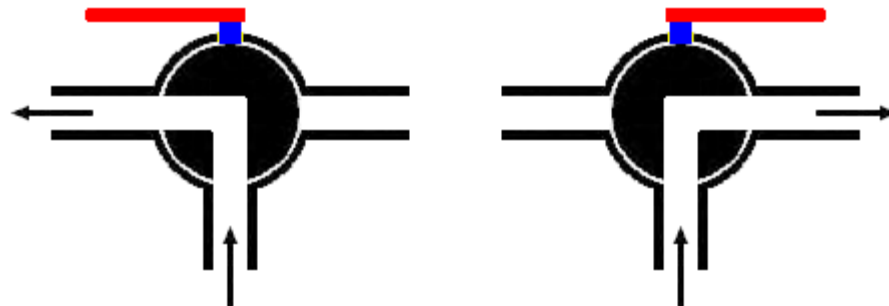
- **Measures to prevent a polymerization reaction runaway due to loss of coolant:**
- **Coolant flow gauge with low-flow alarm**
- **Stirrer rpm gauge with alarm**
- **Stirrer and coolant interlock for monomer addition (inherent safety principle)**
- **Monomer addition stopped if coolant control valve near 100 % open.**
- **Temperature sensors along length of reactor to check for normal profile and upset indication**

Relief Installation Guidelines

- **Industrial standards published by the American Society of Mechanical Engineers (ASME) and by the American Petroleum Institute (API)**
 - **Stress analysis and reaction forces for material flow through relief systems: API standards**
 - **Relief system weight**
 - **Static pressure, pressure changes**


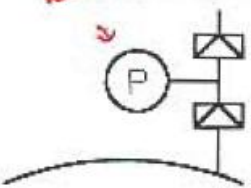
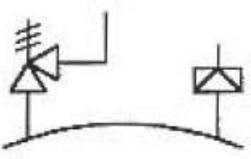
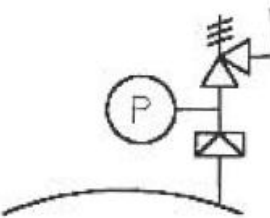
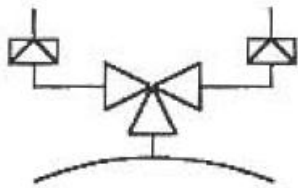
Relief Installation Examples

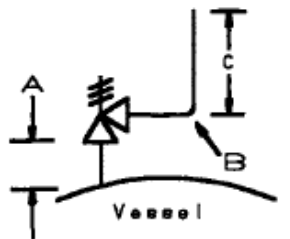
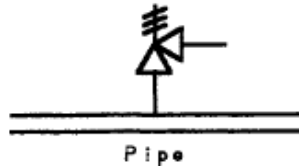

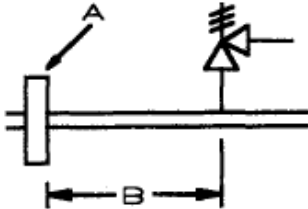
- **Two rupture disks with pressure gauge between to detect for leakage: toxic materials**
- **Two rupture disks connected with 3-way valve to allow maintenance on one disk**
- **Backup rupture disk in parallel with a smaller relief valve set at a lower pressure.**
- **Rupture disk to protect more expensive relief valve with a pressure gauge between them**

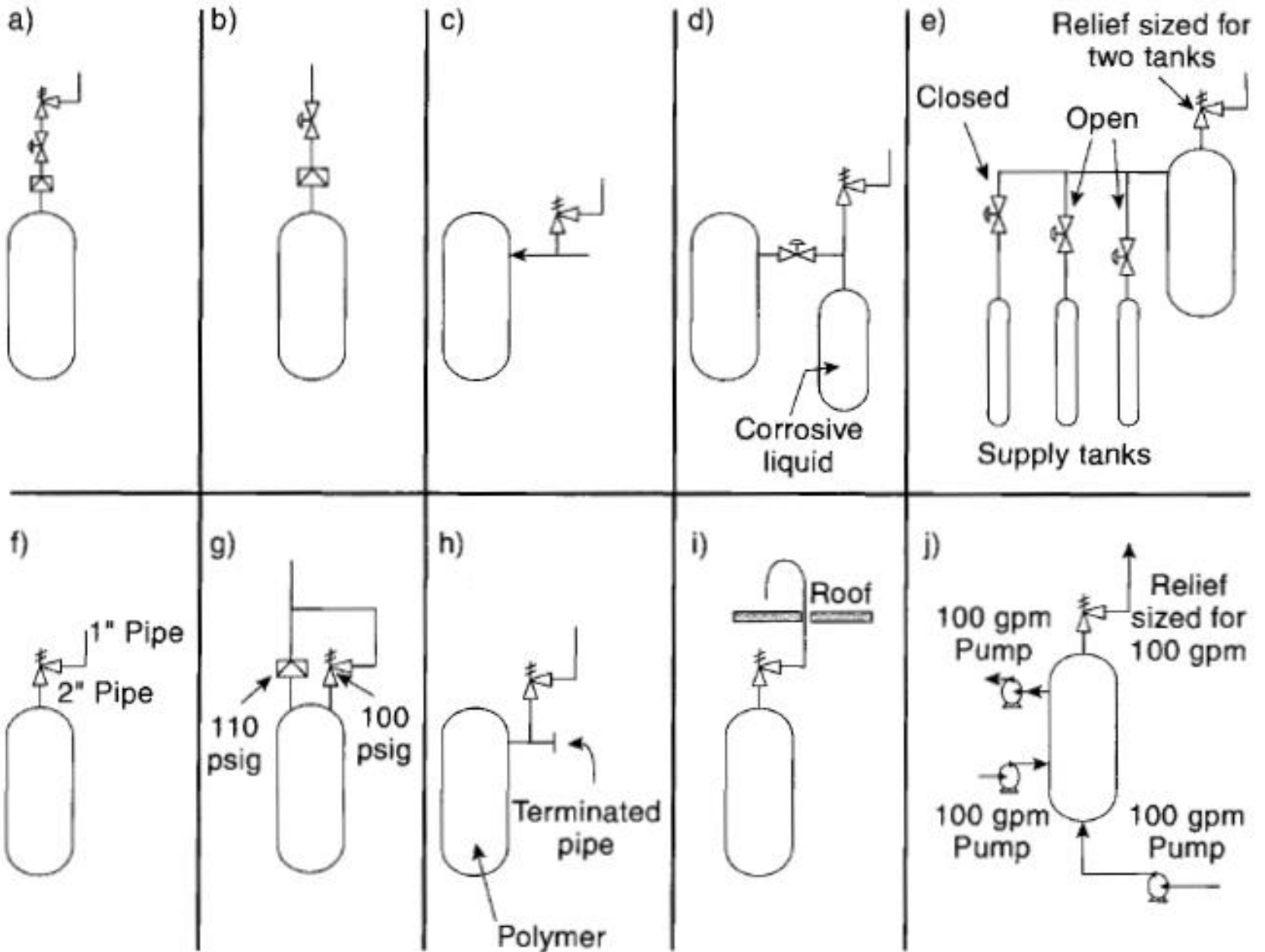


Location Guidelines


- **Relief valves on all vessels**
- **Pressure or vacuum protection for vessels**
- **Steam jackets**
- **Pipes between valves**
- **Pumps, compressors, turbines on discharge**
- **High pressure connected to low pressure**
- **Safety/cost balance: relief device vs design for highest pressure**

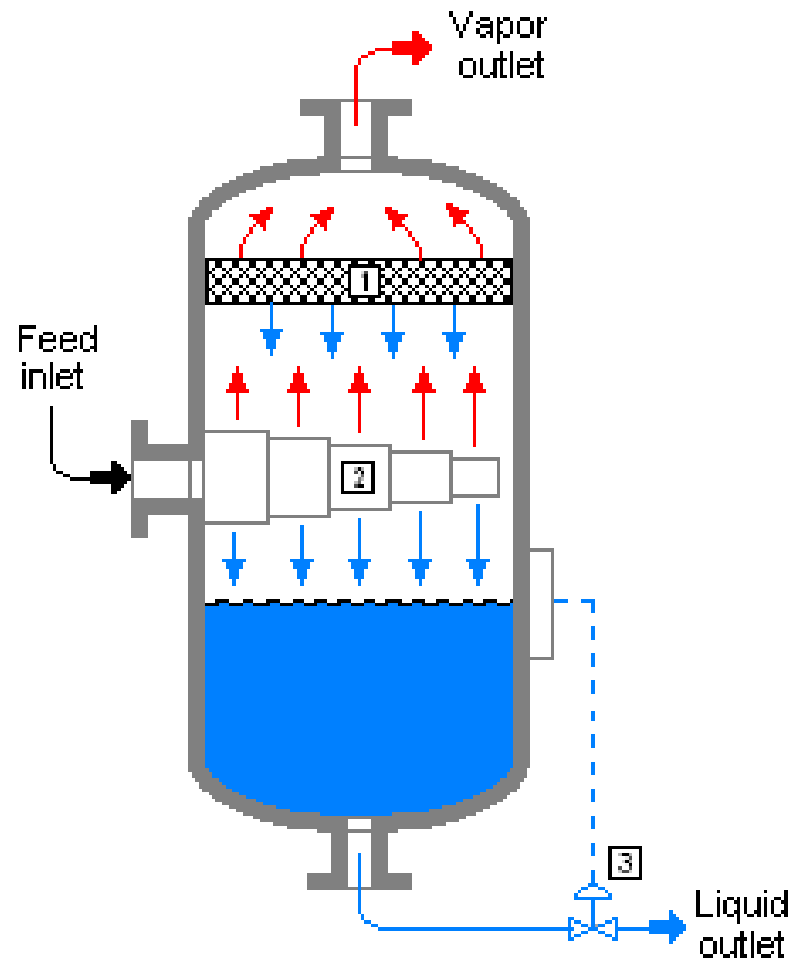
System	Recommendations
 <p>Vessel</p>	<ul style="list-style-type: none"> ● Rupture Disc in Corrosive Service. ● Or for Highly Toxic Materials where Spring Loaded Valve May Weep.
<p><i>tell-tale pressure gauge</i></p> 	<ul style="list-style-type: none"> ● Two Rupture Discs in Extremely Corrosive Service. The 1st May Periodically Need to be Replaced.
	<ul style="list-style-type: none"> ● Rupture Disc and Spring Loaded Relief, Normal Relief May Go Through Spring Loaded Device, and Rupture Disc Is Back-up for Larger Reliefs.
	<ul style="list-style-type: none"> ● Two Reliefs in Series. The Rupture Disc Protects Against Toxicity or Corrosion. The Spring Loaded Relief Closes and Minimizes Losses.
	<ul style="list-style-type: none"> ● Two Rupture Discs with Special Valve Which Keeps One Valve Always Directly Connected to Vessel. This Type Design Is Good for Polymerization Reactors Where Periodic Cleaning Is Necessary.

System	Recommendations												
 <p>Vessel</p>	<p>A. Pressure Drop Not More Than 3% of Set Pressure</p> <p>B. Long Radius Elbow</p> <p>C. If Distance is Greater Than 10 Feet, Weight and Reaction Forces Should be Supported Below the Long Radius Elbow.</p>												
 <p>Pipe</p>	<ul style="list-style-type: none"> ● Orifice Area of a Single Safety Relief in Vapor Service, Should Not Exceed 2% of the Cross Sectional Area of the Protected Line. ● Multiple Valves with Staggered Settings May be Required. 												
	<p>A. Process Lines Should Not be Connected to Safety Valve Inlet Piping.</p>												
	<p>A. Turbulence Causing Device</p> <p>B. Dimension (B) shown below:</p> <table border="1" data-bbox="859 1071 1439 1363"> <thead> <tr> <th>Device Causing Turbulence</th> <th>Minimum Number of Straight Pipe Diameters</th> </tr> </thead> <tbody> <tr> <td>Regulator or Valve:</td> <td>25</td> </tr> <tr> <td>2 Ells or Bends Not in Same Plane:</td> <td>20</td> </tr> <tr> <td>2 Ells or Bends in Same Plane:</td> <td>15</td> </tr> <tr> <td>1 Ell or Bend:</td> <td>10</td> </tr> <tr> <td>Pulsation Damper:</td> <td>10</td> </tr> </tbody> </table>	Device Causing Turbulence	Minimum Number of Straight Pipe Diameters	Regulator or Valve:	25	2 Ells or Bends Not in Same Plane:	20	2 Ells or Bends in Same Plane:	15	1 Ell or Bend:	10	Pulsation Damper:	10
Device Causing Turbulence	Minimum Number of Straight Pipe Diameters												
Regulator or Valve:	25												
2 Ells or Bends Not in Same Plane:	20												
2 Ells or Bends in Same Plane:	15												
1 Ell or Bend:	10												
Pulsation Damper:	10												



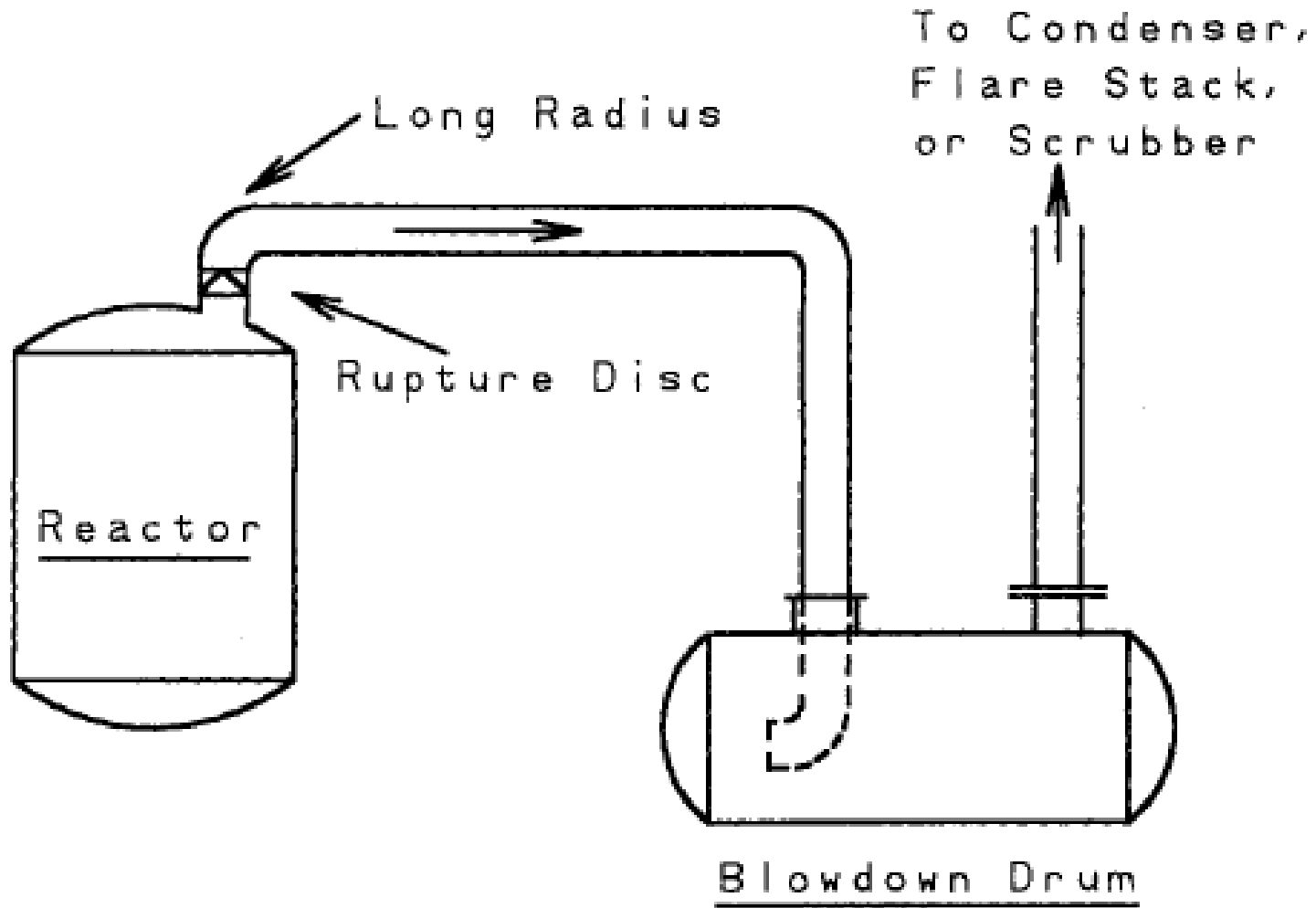
Total Containment Systems

- Relief materials are mostly vented to total containment and treatment systems
- Knockout: separation of liquid from vapor; coolant for high boiling material (Ex 8-3, p. 374) 
- Liquid collected, transferred, incinerated
- Vapor transferred to treatment, e.g., condenser (high boiling), scrubber (toxic), incinerator, flare (combustible, toxic), combination



- 1 De-entrainment mesh pad
- 2 Inlet diffuser (distributor)
- 3 Liquid level control valve





Relief containment system with blowdown drum. The blowdown drum separates the vapor from the liquid

Material Treatment

- **Flares: flammable or toxic materials converted to less hazardous combustion products**
 - Flare design: for a stable flame and a non-hazardous radiation (Ex 8-4, p. 375)
- **Scrubbers: columns for surface contact; convert to less hazardous or more manageable materials**
 - Scrubber examples: caustic bath (H_2S), water (NO_2)



